

# Ammonia Fuel Opportunities, Markets, Issues

Dr. Steve Wittrig Senior Advisor, Advanced Energy Systems Clean Air Task Force (www.catf.us) tswittrig@gmail.com

# The Prize – 21st Century

(With Apologies to Daniel Yergin)

### A zero carbon fuel

That can be used for transportation and power generation

That is scalable from global chemical to global energy proportions

That is an inherently clean fuel with regard to traditional pollutants and CO<sub>2</sub>

That has a century long history of large scale handling and use

That is competitive in energy pricing to current fuels

That holds promise for low or no carbon production (through CCS on standard technology or advanced technology for renewables or nuclear)

That *appears to be* within easy reach through optimization of production, use and safety regulations



### What We Know

- Ammonia average price over last 20 years is \$300 per tonne. Equivalent to \$1.75 gal gasoline and \$14 per MMBTU LNG. Power at \$0.11 per kwh (@45% efficiency)
- Ammonia can be produced from zero carbon energy (hydro, nuclear, wind) and with significant CCS at lowest cost of capture for any hydrocarbon process
- Ammonia diesel engines are proven and essentially equivalent in cost (either with diesel blending, precracking or advanced engines)
- Ammonia turbines with precracking to produce hydrogen for component of the fuel are efficient and flexible

 In general, these technologies have considerable headroom and are primarily in need of engineering optimization and field prototyping for commercialization



### Low Carbon Ammonia (And Front End For CCS)

- Ammonia plants emit pure (sequestration-ready) CO<sub>2</sub>. Approximately 2/3 is pure. With current technology, the rest is flue gas from the reformer.
- There are active markets to purchase CO<sub>2</sub> for enhanced oil recovery.
- Ammonia plants built close to EOR fields can sell their waste CO<sub>2</sub> to be sequestered in oil fields after use. EOR technologies exist for complete CO2 sequestration at low incremental cost. (co-injection with N2)
- This co-product value can reduce production cost for eventual fuel use.
- These operations will also supply a great deal of experience, technology and infrastructure for carbon capture and for CO<sub>2</sub> transportation and sequestration.
- This will serve as a bridge while "green ammonia" technologies from renewables, hydro and nuclear energy are optimized for a decarbonized ammonia energy system for power and for liquid fuel for transportation.



### Zero Carbon Ammonia As a Basis for Affordable, World Scale Zero Carbon Energy

- Decarbonize the giant gas reserves. Initially, pure CO2 injection for miscible EORce. Separate injection points of CO2 flue gas for immiscible pressure maintenance.
- Injection continues into reservoir following oil production and into adjacent reservoirs.
- Renewable energy (wind, solar, hydro, geothermal) and nuclear to produce ammonia from water and air.
- Electrolysis to H2 and Haber Bosch ammonia in development at prototype stage – potentially \$400 per tonne on technologies in development.
- Solid State Ammonia Synthesis (SSAS) also in the same range.
- Fundamental point. Ammonia is the simplest molecule that stores hydrogen in a liquid form at near ambient conditions.



# Power Generation - NH3 Diesel Engines

- One of the most promising early applications for ammonia as a fuel is large stationary diesel gen sets. (nominally 40-45% efficient for power, 75% for CHP). Sturman engines as prototype.
- There are over 200 GW of medium to large diesel engines that run on a continuous basis producing electricity. These installations often feature a dozen or more engines installed in a kind of 'modular power plant'.
- These modular power plants can be installed very quickly, scaled up or added as necessary, and redeployed when not needed or if the economic conditions change.

- Gas Turbines. Crack some of the NH3 to produce arbitrary amount of H2 for co-feed with NH3 (tunable fuel, exhaust heat recovery). SPG
- Fuel Cells. Ideal fuel for SOFCs. Ideal hydrogen storage and delivery for PEMFCs and FCVs
- Space heating, Process heat (similar to LPG). Ideal for CHP from gensets.



# Starting Points For Transportation

- There are several entrepreneurs and institutions that are advancing the technology of engines for ammonia fuel.
- Toyota is developing a technology and patent portfolio for ammonia engines including onboard cracker for tunable addition of hydrogen. <u>https://www.collectiveip.com/companies/toyota-motors/patents?fin=Norihiko+Nakamura&q=ammonia+engine</u>
- Jay Schmuecker has developed a system to manufacture ammonia from solar and a tractor to run on the ammonia. <u>https://nh3fuel.files.wordpress.com/2014/10/nh3fa-2014-jay-schmuecker.pdf</u> <u>http://solarhydrogensystem.com/new/wp-content/uploads/2015/04/schmuecker-launch-brochure-web.pdf</u>
- Sturman Industries is developing ammonia engines based on advanced concepts in valves, camless engines and injection strategies. <u>https://www.youtube.com/watch?v=aojUI74qHfc</u>
- The lowa Energy Center is developing engine technologies for use in agricultural industry.

http://www.iowaenergycenter.org/search/?cx=003074495176662961374%3Apisxjengoxu&cof=FORID%3A11&ie=U TF-8&q=energy+ammonia+engine&sa=Search&sa=Search

 Greg Vezina has developed ammonia vehicles on standard platforms. From all appearances, these are well developed prototypes. <a href="https://www.youtube.com/watch?feature=player\_embedded&v=Bs3HSChSh\_E">https://www.youtube.com/watch?feature=player\_embedded&v=Bs3HSChSh\_E</a> (Hydrofuel, <a href="http://nh3fuel.com/">http://nh3fuel.com/</a>)

## **Global Sources - Overview**

- Alaska North Slope
- US Southwest/Midwest/Fracking in general
- Middle East / North Africa (lowest cost ammonia currently, lots of headroom)
- Canada Hydroelectric (10's of GW of low cost power on contract)
- Iceland (practically unlimited geothermal at ~3 cents/kwh)
- Big Wind (depends on low capex electrolysis tech, allows local grid stabilization)
- Off Peak Nuclear (depends on low capex electrolysis tech, allows local grid stabilization)



# **Global Markets - Overview**

- Alaska (displace diesel across the state, supply Anchorage, alternate export market for Alaska gas)
- Hawaii (displace diesel, resid and gasoline across the islands; CHP and distributed generation)
- Northeast/MidAtlantic (energy security, grid stability, alternative to gas)
- Midwest (energy security, grid stability, displace fuel oil/LPG, fertilizer)
- Caribbean (displace diesel, resid and gasoline across the islands)
- Japan (alternative to expensive LNG and coal, replacing nuclear)
- Indonesia (displace diesel, resid and gasoline across the islands)
- China (clean cities, rural access, much easier than gas)
- Europe (energy security, CHP, DG, fertilizer/fuel)
- Africa, South America (ammonia diesel gen, clean cities, rural access)

### Neighborhood Energy Station

- A typical high volume gasoline station can easily dispense 1.5 MM gallons of multiple grades of gasoline/diesel in a year. This case examines a 'neighborhood' ammonia energy station of approximately the same scale that could provide power and heat to the neighborhood (or condo or office building) in an urban environment. This station would house a diesel genset/CHP unit running on ammonia. The prototype for this is the MHI MegaNinja gas genset (delivered on 40' trailer, 1.5 MW generator operating at 42.5% efficiency, designed for combined heat/power taking efficiency up to 75% for medium pressure steam/space and water heating and adsorptive air conditioning.)
- The general complexity of these stations would be less than a gasoline station (single grade, dispensed almost entirely to the generators instead of retail interface with hundreds of transactions to untrained public per day). Tank volume, general regulatory requirements and fuel delivery logistics would be similar.
- The average weekly volume would be about 35,000 gallons. We can 'design' for 40,000 gal/week peak usage. A typical tank size for ammonia distributors is 30,000 gallons. So, with one 30,000 gal tank (installed underground for safety, security and ease of temp/pressure maintenance), we could operate with three a week deliveries from 11,500 gal tank trucks (typical size ammonia trucks). I'm sure the logistics can/will be optimized beyond that, but this will do for illustration.
- Very rough project costs would be about \$1.2 MM for ammonia MegaNinja, \$0.1 MM for underground tank, connections and land. Roughly \$1.5-\$2 MM.



### Neighborhood Energy Station

- Upside revenue potential for similar projects in other regions of the world. Examples:
- Island economies that must generate their power from fuel oil (Hawaii, Caribbean, Indonesia). Fuel oil is \$30-\$40 per mmbtu. It is dirty and must be located away from populations (and especially resorts). That also makes it very difficult to capture and utilize the 1/3 of the btu's from CHP that clean ammonia engines can provide. These units can provide clean power at less than half the cost and, on top of that, very efficient heat and air conditioning (absorptive chilling).
- Medium scale distribution/retail (frozen/refrigerated foods), light industry and agriculture utilizing refrigeration, medium pressure steam or drying (e.g., crops) that place high value on the associated heat)
- Regions that place high value on pure water (exhaust from ammonia Sturman engine is water and nitrogen. Pure water can be captured at the cost of condensing the water.) Combustion of 1.75 MM gallons of ammonia generates about 1.7 MM gallons of water.
- They will be very attractive to sites willing and able to pay large premiums for locally controlled, uninterruptible power (financial/business centers, server farms, hospitals, military/government installations, large research facilities/research universities)
- Regions that are imposing a cost on CO2 emissions can reduce or eliminate those costs. Clean Power Plan.
- Grid ancillary services. Load following, Peak power, Voltage/frequency regulation, Locational value, Black start



### Neighborhood Energy Station – Ideal Power







### Utility Level Storage to Stabilize Grid

### **Utility Storage Market Drivers:**

- Wind and Solar Integration
- Energy Arbitrage
- Frequency Regulation & Ancillary Services
- Infrastructure Upgrade Deferral
- Locational Capacity

Different battery technologies will supply this market



**120kW – 500kW** Bonneville Power Authority, WA

### Ideal Power is forming alliances with leading battery suppliers











### Ammonia Energy Station can be installed at highest locational value Highest leverage to stabilize grid, relieve congestion and defer infrastructure investment

For Each DPA & Substations/Feeders Annual Dist. Planning & Integration Capacity Analyses Biennial DRP Locational Value Analysis







http://resnick.caltech.edu/docs/MTS\_V2.pdf

### Neighborhood Energy Station

- With a set up like Ideal Power, this configuration can
- Easily accommodate renewable solar or wind by cutting back genset (with immediate local load following).
- Pass through solar/wind or ammonia power and ancillary services to the grid. 24/7 availability of peaking power (125% of genset rating typical), frequency regulation, voltage support, black start.
- Provide predictable, addressable standby reserve available on 5 minute call-up (with right incentives and minimally sophisticated 'smart grid' controls) (much cheaper and much more flexible than spinning reserve CCGT that is only used as gas prices are rising above \$40/mmbtu)
- Provide distributed and potentially very substantial regional fuel reserve for mid-winter, late summer, regional security (much cheaper (pseudo-'free') than natural gas storage and much more flexible). 30,000 gallon underground tank of ammonia provides about 180 MWh of electricity (42%) and 400 MMBTU of CHP heat (30%), About 5 days of continuous operation.



# How Does This All Get Started?

- Market demonstration at 1-10 MW scale (diesel gen, refit, new optimized, blends)
   Sturman engines, Fleming Ammonia, others
- Evaluation of these systems for zero carbon power across the value chain by experts and system modelers
- Engage regulators and power industry
- Engage ammonia producers/investors
  - New build guaranteed offtake (some fraction of production)
  - Eventually, utility plants with guaranteed returns for fuel take or pay (with perhaps shared profits for joint sales into market after satisfaction of energy market contractual requirements)
  - Market, regulatory, technology demo support from self selected producers
  - Plant technology/engineering firms (KBR, Uhde, MHI, etc) that will benefit from increased building
- Low cost, high CO2 value areas for low carbon, low cost fuels
- Accelerate demo/commercialization of power to NH3 technologies
  - Compile list of potentially interested investors, green funding, etc for incipient technologies for investments in the range of \$5-\$20 MM for FEED, critical demoes or initial deployment in regions for low cost "stranded" power (i.e., Canada, Iceland, Hawaii)
  - Competition for proposals for ammonia from power, perhaps with funding from such entities
- Project development with engaged stakeholders



# **Backup Slides**



# Indicative Economics - Overview

- New world scale plant, 1 mm tonnes/year @ \$1200 per tonne of annual capacity. 10% annual capital charge about \$120/tonne
- Approx. 30 mmbtu of gas required per tonne of ammonia (e.g., \$4/mmbtu gas, about \$120/tonne of ammonia)



http://www.ourenergypolicy.org/wp-content/uploads/2015/04/BNEF\_ChemicalsWhitePaper\_2015-01-20-final1.pdf



## **Compare to Battery Storage**

- Much lower cost, 30,000 gal underground tank (similar to gas station) stores about 180 MWh and 400 MMBTU CHP heat. About \$100,000 capital cost.
- Much longer life (genset versus batteries)
- Gensets require more maintenance
- Zero carbon 'recharge' from ammonia delivery (does not use local excess power to manage local peaks/valleys). Accesses lowest cost excess power in region.



# Compare to Nat Gas Genset

- No need for gas supply
- No new pipelines required (multi hundred million \$ projects, 5 year projects from negotiation thru gas flow, political/public opposition)
- Purchase fuel from multiple sources rather than prices set by pipeline operations
- Reduced exposure to price volatility
- Not subject to pipeline/compressor failure
- Very low cost local storage of energy (days of operation without refill) compared to expensive cavern storage backed up by LNG
- No CO2 emissions
- Low/No NOX



Because the system can now operate at variable rpm, it maintains a high torque regardless of the output, thus maintaining near full-load efficiency throughout its operating range. Additionally, more output can be derived from the same engine if it can be operated to the higher rpm, that is, beyond the typical synchronous speed of 1800 rpm. Another advantage is that the same machine can be applied to the 50 Hertz market, without de-rating or design changes.



Er	ngine/Ger	nerator Out	put	. Ν	De	elivered l	٢N
RPM	Volts	Freq (hz)	KW		Volts	Freq (hz)	
1000	98	135	39	Power \	480	60	
2200	207	297	93	Conversion /	480	60	
3000	258	405	130		480	60	
				V ·			

FIGURE 1. CONCEPTUAL DESIGN OF INVERTER-BASED ENGINE GENERATOR



37 88 123

http://bpe-ne.com/wp-content/uploads/2012/07/top10-reasons-to-choose-inverter-based-engine-chp.pdf

Ammonia Fuel Cost Cap Charge	Ammonia Cost (\$/tonne) \$ 300 Capex for dieselgen (\$/kw)	\$/mmbtu (@21.3 mmbtu per tonne) \$ 14.08 % premium utilization per year	Efficiency of conversion to power 45.0% premium kwh per year per installed kw	kwh per tonne of ammonia 2812.5 Annual capital charge as % capex	kwh per gallon of ammonia 6.53 Annual capital charge (per kw)	\$/kwh for fuel cost \$ 0.107 capital charge per premium kwh		Total Capital \$ 2,250,000	Annual Operating Profit (no cap charge) \$ 503,758	Payback, years 4.47
	\$ 1,500	60.0%	capacity 5256	12.5%	\$ 188	\$ 0.036				
Scale of Installation and costs	Scale (kw installed)	premium kwh dispatched	annual tonnes of ammonia for premium ops	Annual fuel expenditure for premium ops, \$	Annual Capex Charge, \$	annual gallons of ammonia	ammonia use during full dispatch (gal per hour)	Days of operation from full 50,000 gal tank	number of 11500 gal tanker truck deliveries per year	Annual maintenance and labor @ \$0.02 per kwh
	1500	7,884,000	2803	\$ 840,960	\$ 281,250	1208179	230	9.1	105	\$ 157,680
Revenue Streams	Recoverable heat per tonne of ammonia (40% of 21.3 MMBTU)	Total recoverable heat, mmbtu	Sales heat price, \$/mmbtu	Annual heat revenue		Sales power price, premium on demand, \$ per kwh	Annual power revenue (from % utilization)		Total annual revenue Premium operation	Premium Revenue - fuel cost - cap charge - labor & maintenance
	8.5	23827.2	\$ 4.00	\$ 95,309		\$ 0.15	\$ 1,182,600		\$ 1,277,909	\$ (1,981)
Opportunistic operations	Sales power price, opportunistic, \$/kwh	Opportunistic sales (% dispatch outside premium window)	Opportunistic dispatch (hrs/yr)	Opportunistic dispatch (kwh/yr)	Annual tonnes ammonia for opportunistic	Opportunistic fuel/maintenance cost	Opportunistic revenue (power+heat)	Opportunistic revenue - fuel/maintenance	Total annual revenue (w/ opportunistic)	Total Revenue - fuel cost - cap charge - labor & maintenance
	\$ 0.20	50%	1752	2,628,000	934	\$ 332,880	\$ 557,370	\$ 224,490	\$ 1,835,278	\$ 222,508



							Ch4				
Capital	Capacity		Longth	Sustaining	CADEV	Cash	mmbtu	Gas			
(MM	(1000	Cost of	of loan,	capital MM	charge	ch4 per	tonne	per			
\$)	tpa)	Capital	years	per year	annual MM	tonne	NH3	mmbtu			IRR
1100	1200	4.0%	20	\$ 10.00	(\$70.94)	\$45.00	32	\$3.00			12.3%
Gas		NH3							CO2		
cost		sales						Pure	sales	CO2	
per	Cash cost	price \$		Cash	Profit, cash -			CO2,	price, \$	revenu	Profit
year	per year	per	Revenue	Margin	cap charge			1000	per	es,	with
MM\$	MM	tonne	(MM \$)	MM\$	MM\$			tpa	tonne	MM\$	CO2
\$ 115	\$ 169	\$ 300	\$ 360	\$ 191	\$ 120			1500	20	\$ 30	\$ 150



### Some Initial Scenarios For Discussion



			Haw	aii distillate	, resid and o	oal import	(125 T BTU)					
MOD	DEL RESI	JLTS				COST, T	HERMO AND CO2	MATRIX				
USER INPUTS ALLOWED IN GREEN CELLS	ALL VALUES EQUIV 1	ALL VALUES CORRESPOND TO CASE PARAMETERS		AMMONIA	NATURAL GAS	GASOLINE	LPG	DIESEL	COAL	ETHANOL	METHANOL	DME
REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4	1.00	5.86E+06		INPUT Price of NH3 delivered to site, \$ per tonne	INPUT Price of gas delivered to site, \$ / mmbtu	INPUT Price of gasoline delivered to site, \$ / gal	INPUT Price of LPG delivered to site, \$ / gal	INPUT Price of diesel delivered to site, \$ / gal	INPUT Price of coal delivered to site, \$ / tonne	INPUT Price of ethanol delivered to site, \$ / gal	INPUT Price of methanol delivered to site, \$ / tonne	INPUT Price of DME delivered to site, \$ / tonne
OPTIONAL USER- DEFINED VARIABLE. ENTER VARIABLE NAME IN THIS CELL ENTER (1 T NH3 BASIS) IN CS. ITERATE DA TO ACHEVE DESIRED QUANTITY IN DS		0.00		\$350	\$30.00	\$4.00	\$4.00	\$4.00	\$50	\$5.00	\$200	\$290
MMBTU (or 1000 CF gas equiv) contained in NH3	21.32	124,987,434		Tonnes NH3 for 21.3 MMBTU	MMBTU gas for 21.3 MMBTU	Gal gasoline for 21.3 MMBTU	Gal LPG for 21.3 MMBTU	Gal diesel for 21.3 MMBTU	Tonnes coal for 21.3 MMBTU	Gal ethanol for 21.3 MMBTU	Tonnes methanol for 21.3 MMBTU	Tonnes DME for 21.3 MMBTU
MMBTU gas required for NH3	32.0	187,616,000		14	21.3	172	234	156	10	253	0.982	0.71
TCF natural gas required for NH3	2.946-08	0.172		NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario	Gas Fuel Cost (for 21.3 mmbtu) - This Scenario	Gasoline Fuel Cost (for 21.3 mmbtu) - This Scenario	LPG Fuel Cost (for 21.3 mmbtu) - This Scenario	Diesel Fuel Cost (for 21.3 mmbtu) - This Scenario	Coal Fuel Cost (for 21.3 mmbtu) - This Scenario	Ethanol Fuel Cost (for 21.3 mmbtu) - This Scenario	Methanol Fuel Cost (for 21.3 mmbtu) - This Scenario	DME Fuel Cost (for 21.3 mmbtu) - This Scenario
Tonnes water produced from NH3	1.586+00	9,263,540		\$350	\$639	\$688	\$936	\$624	\$52	\$1,265	\$196	\$206
# Global ammonia industry	6.672-09	0.039		kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 like)	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 like)	kwh from 21.3 mmbtu at 35% efficiency (coal like)	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 like)	kwh from 21.3 mmbtu at 35% efficiency (coal like)	kwh from 21.3 mmbtu at 35% efficiency (coal like)	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 like)	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3
II of World Scale NH3 Plants	1.258-06	7.33		280	2800	2200	2800	2200	2200	2800	280	2800
Number of 60,000 cbm vessels	2.44E-05	143		Fuel cost for power, \$/kwh from NH3	Fuel cost for power for power, \$/kwh from gas	Fuel cost for power, \$/kwh from gasoline	Fuel cost for power, \$/kwh from LPG	Fuel cost for power, \$/kwh from diesel	Fuel cost for power, \$/kwh from coal	Fuel cost for power, \$/kwh from coal	Fuel cost for power, \$/kwh from methanol	Fuel cost for power, \$/kwh from DME
Number of 80 tonne railcar deliveries	0.0125	73,288		\$0.125	\$0.228	\$0.313	\$0.334	\$0.284	\$0.024	\$0.452	\$0.070	\$0.074
# of 1 MM TPA NH3 pipeline	1.005-06	5.9	AMMONIA, NO CCS	AMMONIA w/ HARVEST	NATURAL GAS	GASOLINE	LPG	DIESEL	COAL	ETHANOL	METHANOL	DME
MWh from 45% efficient power plants	2.818+00	16,475,030	T CO2 per 21.3 mmbtu,only	T CO2 per 21.3 mmbtu,only production,	T CO2 per 21.3 mmbtu, NOT COUNTING	T CO2 per 21.3 mmbtu, NOT COUNTING	T CO2 per 21.3 mmbtu, NOT COUNTING	T CO2 per 21.3 mmbtu, NOT COUNTING	T CO2 per 21.3 mmbtu, NOT COUNTING	T CO2 per 21.3 mmbtu, NOT COUNTING	T CO2 per 21.3 mmbtu, NOT	T CO2 per 21.3 mmbtu, NOT
# of 10 MW plants that can be run for 1 year, 45%	3.218-05	188.0	1.93	0.68	1.23	1.65	1.48	1.68	2.42	0.33	1.80	1.80
Equivalent # of 6 mtpa LNG train (BTU basis)	6.87E-08	0.40				CASE	NOTES					1
Tonnes LNG equivalent	0.41	2,403,830	HAWAII d	istillate, res	id and coal	import (125	T BTU)					
Metric Tonnes coal equiv	1.04	6,097,520										
Tonnes oil equivalent (TOE)	0.500	2,931,500	Gas price -	\$40 per mmb	otu							
Tonnes resid equiv	0.530	3,107,390	Power - \$3	50 per mwh (	about 80% fro	om coal, resid	and fuel oil)					
Gal LPG equiv	234	1,371,942,000	This could I	oe displaced i cargo shin de	by 6 mmt nn3 liveries per ve	(about 7.5 ar	nmonia plant	s)				
Gal Gasoline equiv	172	1,008,436,000	Fuel cost fo	or ammonia p	er vear - \$2.0	bb. Fuel cost	for power ('fr	ree' heat fron	n CHP) - <b>\$12</b> 5	per		
Gal Ethanol equiv	253	1,483,339,000	MWH.						,			
Price NH3	\$350		Fuel cost fo	or gas per yea	r- \$3.7	bb. Fuel cost	for power ('fr	ree' heat fron	n CHP) - \$228	8 per MWH.		
Total NH3 cost \$		2,052,050,000	Fuel cost fo	or diesel per y	ear - \$3.6	bb. Fuel cost	for power ('fr	ee' heat from	n CHP) - <b>\$28</b>	4per		
Fuel cost for power, \$/kwh from NH3	\$ 0.125		Evel cost fo	or coal per ve	ar. \$0.3 l	hh. Fuel cost f	for nower ('fre	ee' heat from	CHD) - \$30	) per MWH		
Price NATURAL GAS	\$30.00		ruercostre	n courper ye	ai	55.146166561	ion power ( in	ce near nom	¢30	per mini		
Total Natural Gas cost \$		\$ 3,746,457,000	Fuel price r	not the whole	story.							
Fuel cost for power for power, S/kwh from gas	\$ 0.228		Ammonia r	nuch easier te	o distribute ar	nd store than	coal or gas.					
Price GASOLINE	\$4.00		Ammonia r	nuch cleaner	to burn and u	ise than coal,	resid or fuel o	oil.				
Total Gasoline cost \$		\$ 4,033,744,000	Ammonia of Se	an be deploy	ed for power kw. With tur	gen at 40%+ n on/off in a f	efficiency at s	cales betwee	n 250 kw and	50 M. At a		
Fuel cost for power, \$/kwh from gasoline	\$ 0.313		Small scale	, clean combu	ustion (500 kv	v – 200 MW)	greatly facilita	ates CHP (hea	ting, absorpti	ive AC, hot		
Price LPG	\$4.00		water). Rai	sing efficienc	y to 70-80% a	nd displacing	other heating	g fuels (perha	ps 50% additi	onal to		
Total LPG cost \$		\$ 5,487,768,000	electricity.	+ \$250 - \$250	) por toppo is	available from	n \$2.\$4 and a	round the we	rld for this on	tiro markat		
Fuel cost for power, S/kwh from LPG	\$ 0.334		once the de	emand is esta	blished. That	existing dem	and for fuel c	oil, LPG, LNG ł	nas establishe	d much		
Price DIESEL	\$4.00		higher price	es.								
Total Diesel cost \$		\$ 3,658,512,000										
Fuel cost for power,	\$ 0.284											
Price COAL	\$50											
Total Coal cost \$		\$ 304,876,000										
Fuel cost for power,	\$ 0.024											
Price ETHANOL	\$5.00											
Total Ethanol cost \$		\$ 7,416,695.000										
Fuel cost for power,	\$ 0.452											

#### Hawaii resid/distillate

Most of Hawaii's electricity is generated from heavy hydrocarbons. This is expensive (HI power more than 3X cost of mainland) and environmentally destructive, 35-40 cents/kwh). Hawaii is working very hard to reduce hydrocarbon reliance (small scale LNG, renewables energy efficiency).

There is great scope for this since power is so expensive. But the cheapest way is through ammonia.

Displacing all of HI resid, fuel oil and coal about equivalent to 6 MMTPA NH3 (about 7 plants or 140 cargo ship deliveries.) Ammonia at \$350/tonne has a fuel cost of 13 cents / kwh (not counting credit for CHP from ammonia diesel gen sets).

Think also – Caribbean, Indonesia, Greece, Philippines



NEIC	GHBC	RHOOD ENE	RGY STATI	ON (LIKE A	GAS STATIO	N) Dispensi	ng 1.75 MM	Gals Per Ye	ar Of Amm	onia		
мо	DEL RESU	JLTS				COST, T	HERMO AND CO2	MATRIX				
USER INPUTS ALLOWED IN GREEN CELLS	ALL VALUES EQUIV 1 MT NH3	ALL VALUES CORRESPOND TO CASE PARAMETERS		AMMONIA	NATURAL GAS	GASOLINE	LPG	DIESEL	COAL	ETHANOL	METHANOL	DME
REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4	1.00	4,060		INPUT Price of NH3 delivered to site, \$ per tonne	INPUT Price of gas delivered to site, \$ / mmbtu	INPUT Price of gasoline delivered to site, \$ / gal	INPUT Price of LPG delivered to site, \$ / gal	INPUT Price of diesel delivered to site, \$ / gal	INPUT Price of coal delivered to site, \$ / tonne	INPUT Price of ethanol delivered to site, \$ / gal	INPUT Price of methanol delivered to site, \$ / tonne	INPUT Price of DN delivered to site, 5 / tonne
OPTIONAL USER- DEFINED VARIABLE. ENTER VARIABLE NAME IN THIS CELL, ENTER (1 T NH3 BASIS) IN CS. ITERATE ON TO ACHEVE DESIRED QUANTITY IN DS		0.00		\$350	\$15.00	\$3.00	\$2.00	\$3.80	\$50	\$3.00	\$200	\$290
MMBTU (or 1000 CF gas equiv) contained in NH3	21.32	86,558			MMBTU gas for 21.3 MMBTU	Gal gasoline for 21.3 MMBTU	Gal LPG for 21.3 MMBTU	Gal diesel for 21.3 MMBTU	Tonnes coal for 21.3 MMBTU	Gal ethanol for 21.3 MMBTU	Tonnes methanol for 21.3 MMBTU	Tonnes DME for 21.1 MMBTU
MMBTU gas required for NH3	32.0	129,930		11	21.1	172	234	4 154	: 1J	25	0.982	a:
TCF natural gas required for NH3	2.946-08	0.000		NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario	Gas Fuel Cost (for 21.3 mmbtu) - This Scenario	21.3 mmbtu) - This Scenario	LPG Fuel Cost (for 21.3 mmbtu) - This Scenario	Diesel Fuel Cost (for 21.3 mmbtu) - This Scenario	Coal Fuel Cost (for 21.3 mmbtu) - This Scenario	21.3 mmbtu) - This Scenario	(for 21.3 mmbtu) - This Scenario	21.3 mmbtu) - This Scenario
Tonnes water produced from NH3	1.588+00	6,415		\$350 kwh from 21.3 mmbtu ai	\$320	\$516	\$468 kwh from 21.3 mmbtu at	\$593	\$53	\$759 kwh from 21.3 mmbtu at	\$196	\$20 kwh from 21.3
# Global ammonia industry	6.672-09	0.000		45% efficiency (gas/nh3 like)	45% efficiency (gas/nh3 like)	kwh from 21.3 mmbtu at 35% efficiency (coal like)	45% efficiency (gas/nh3 like)	kwh from 21.3 mmbtu at 35% efficiency (coal like)	kwh from 21.3 mmbtu a 35% efficiency (coal like)	45% efficiency (gas/nh3 like)	mmbtu at 45% efficiency (gas/nh3	mmbtu at 45% efficiency (gas/nh3
# of World Scale NH3 Plants	1.258-06	0.01		280	2800	2200	2800	220	220	280	2800 Fuel cost for power,	28
Number of 60,000 cbm vessels	2.448-05	0		Fuel cost for power, S/kwh from NH3	Fuel cost for power for power, S/kwh from gas	Fuel cost for power, S/kwh from gasoline	Fuel cost for power, \$/kwh from LPG	Fuel cost for power, S/kwh from diesel	Fuel cost for power, \$/kwh from coal	Fuel cost for power, S/kwh from coal	S/kwh from methanol	Fuel cost for power, S/kwh from DME
Number of 80 tonne railcar deliveries	0.0125	51		\$0.125	\$0.114	\$0.235	\$0.167	\$0.269	\$0.024	\$0.271	\$0.070	\$0.07
pipeline	1.008-06	0.0	CCS T CO2 per 21.3	HARVEST T CO2 per 21.3	NATURAL GAS	GASOLINE T CO2 per 21.3 mmbtu,	LPG T CO2 per 21.3 mmbtu,	DIESEL T CO2 per 21.3 mmbtu,	COAL T CO2 per 21.3 mmbtu,	ETHANOL T CO2 per 21.3 mmbtu,	METHANOL T CO2 per 21.3	DME T CO2 per 21.3
power plants	2.818+00	11,410	mmbtu,only production, no CCS	mmbtu,only production, CO2 harvest	NOT COUNTING UFECYCLE	NOT COUNTING LIFECYCLE	NOT COUNTING UFECYCLE	NOT COUNTING LIFECYCLE	NOT COUNTING UFECYCLE	NOT COUNTING UFECYCLE	mmbtu, NOT COUNTING LIFECYCLE	mmbtu, NOT COUNTING LIFECYCL
can be run for 1 year, 45%	3.218-05	0.1	1.93	0.68	1.23	1.65	1.48	1.68	2.42	0.33	1.80	1.8
Equivalent II of 6 mtpa LNG train (BTU basis)	6.878-08	0.00	1		1.75 14- 0-1-0-	CASE	NOTES					
Tonnes LNG equivalent	0.41	1,665	A typical high y	volume gasoline st	tation can easily d	issense 1.5 MM g	allons of multiple	grades of gasoline	/diecel in a year	This case		
Metric Tonnes coal equiv	1.04	4,223	examines a 'ne	ighborhood' amn	nonia energy statio	on of approximate	ly the same scale	that could provid	e power and heat	to the		
Tonnes oil equivalent (TOE)	0.500	2,030	ammonia. The	prototype for thi	s is the MHI Mega	Ninja gas-driven g	enset (delivered o	on 40' trailer, 1.5 I	MW generator op	erating at 42.5%		
Tonnes resid equiv	0.530	2,152	adsorptive air o	conditioning.)	a near/power tak	ing enciency up o	o 75% for median	r pressure steamy	space and water i	reating and		
Gal LPG equiv	234	950,116	The general con	mplexity of these	stations would be	e less than a gasoli	ne station (single	grade, dispensed	almost entirely to	the generators		
Gal Gasoline equiv	172	698,376	and fuel delive	ry logistics would	be similar.		a paone per augy.	but tank volume,	generarregalator	y requirements		
Gal Ethanol equiv	253	1,027,262	The average we	eekly volume wou	ild be about 35,00	0 gallons. We car	design' for 40,0	00 gal/week peak	usage. A typical t	ank size for		
Gal Ethanol equiv	253	1,027,262	The average we	eekly volume wou ibutors is 30.000 g	Id be about 35,00 allons. So, with o	0 gallons. We can ne 30.000 gal tan	'design' for 40,00 k (installed under	00 gal/week peak ground for safety.	usage. A typical t security and ease	ank size for of		
Price NH3	\$350		temp/pressure I'm sure the log	maintenance), w	e could operate w optimized beyond	ith three a week of that, but this will	eliveries from 11 do for illustration	,500 gal tank truck	ks (typical size am	monia trucks).		
Total NH3 cost \$		1,421,114	Very rough pro	oject costs would	be about \$1.2 MM	A for ammonia M	egaNinja, \$0.1 M	M for undergrour	id tank, connectio	ons and land.		
Fuel cost for power, \$/kwh from NH3	\$ 0.125		Roughly \$1.5-\$	2 MM.								
Price NATURAL GAS	\$15.00		With these deli would be availa	ivery assumptions able 100% of the f	(1.75 MM gal am time (minus maint	monia/year), a 1.5 enance) and could	5 MW Meganinja d be run at the cos	can be supplied 8 st of more freque	5% of the time (.1 nt ammonia delive	3/.15). The unit tries. We can		
Total Natural Gas cost \$		\$ 1,297,274	model this as									
Fuel cost for power for power, S/kwh from gas	\$ 0.114		A CHP unit that offered at belo	t is integrated into w cost/value of lo	the local electric cal power and he	al grid, sells exces at supply. For exa	s power into the g mple, buying low	rid and buys pow cost base load pov	er from the grid w wer at night from	rhen power is utility based on		
Price GASOLINE	\$3.00		TOD pricing and	d operating durin	g the day to ease	peak power dema	nd on the utility's	peakers)				
Total Gasoline cost \$		\$ 2,095,128	Runs 85% of th the mmbtu's in	e time routinely ( the 1.75 mm gal	providing 1.5 MW of ammonia)). W	for 7450 hrs for 1 e will assume con:	1,200,000 kwh an servatively that 15	nd 26,000 mmbtu 5,000 mmbtu of th	of CHP heat (calcu nat heat would be	lated as 30% of effectively used		
Fuel cost for power, S/kwh from gasoline	\$ 0.235		or sold.									
Price LPG	\$2.00		At \$300/tonne,	, 1.75 mm tonnes	of ammonia costs	\$1.2 MM						
Total LPG cost \$		\$ 1,900,232	If we assume N residential cust	lew England/Mide tomers (especially	dle Atlantic urban conservative in t	environments, the he winter). Sales (	or avoided costs of	and \$14 per MMB of gas/power pure	TU are conservati hases) of the pow	ve prices for ver and CHP heat		
Fuel cost for power, S/kwh from LPG	\$ 0.167		from 85% oper	ation at these pri-	ces would yield \$1	57 MM for powe	r and \$0.21 MM f	or heat for a total	of \$1.78 MM.			
Price DIESEL	\$3.80		At \$300/tonne year that kwh a	ammonia, the fue are valued at high	el cost for power ( er than \$0.11 per	even rejecting all kwh, the generato	the CHP heat) is \$ or can be operated	0.107 per kwh. So d for additional pr	o, for the addition ofit. For example	al 15% of the , in New		
Total Diesel cost \$		\$ 2,406,961	England/Middle of a year (1300	e Atlantic region, hrs), we are selli	retail electricity p ng 2,000,000 kwh	rices are uniforml at a margin of \$0.	y above \$0.16 per 05 (bringing in \$1)	kwh. So, if we ar 00,000 extra reve	re running a 1500 nue).	kw unit for 15%		
Fuel cost for power, S/kwh from diesel	\$ 0.269		Overview on ve	ery rough number	s running the busi	iness blind (i.e, sel	ling at average pr	ices, managing CH	IP heat and extra	power sales		
Price COAL	\$50		loosely) Fuel cost at \$30	00/tonne - \$1,200	,000							
Total Coal cost \$		\$ 211,137	Revenues from Opportunistic s	85% base operat sales of power for	ions (contracted a other 15% of gen	t conservative pri erating capacity –	ces) - \$1,780,000 \$100,000					
Fuel cost for power, S/kwh from coal	\$ 0.024		Operating mar	gin of \$680,000 t	o cover capex/op	ex/profit.						
Price ETHANOL	\$3.00		Upside potenti	al on these reven	ues.							
Total Ethanol cost \$		\$ 3,081,787	Capacity payme whether the un	ents from PJM RP nit is running or n	M (market to pay ot). This is \$73,00	for guaranteed ca 0 per year.	pacity in PJM grid	l). In New York, th	iis is about \$200 p	er MW (paid		
Fuel cost for power, S/kwh from ethanol	\$ 0.271		Potential paym	ents from reliabil	ity premiums from	n the grid (this pow	wer is much more	reliable than grid	provided power (	no risk from gas		
MegaTonnes CO2 saved with NH3 with harvest vs	5.506-07	0	deliverability, d	downed power lin	es, frozen equipm	ent, price spikes f	rom hot summer	afternoons, etc).				

#### Local Energy Station Dispensing 1.75 Mm Gals Per Year Of Ammonia

A typical high volume gasoline station can easily dispense 1.5 MM gallons of multiple grades of gasoline/diesel in a year. This case examines a 'neighborhood' ammonia energy station of approximately the same scale that could provide power and heat to the neighborhood (or condo or office building) in an urban environment. This station would house a diesel genset/CHP unit running on ammonia. The prototype for this a gas-driven genset (delivered on 40' trailer, 1.5 MW generator operating at 42.5% efficiency, designed for combined heat/power taking efficiency up to 75% for medium pressure steam/space and water heating and adsorptive air conditioning.)

The general complexity of these stations would be less than a gasoline station (single grade, dispensed almost entirely to the generators instead of retail interface with hundreds of transactions to untrained public per day). But tank volume, general regulatory requirements and fuel delivery logistics would be similar.

The average weekly volume would be about 35,000 gallons. We can 'design' for 40,000 gal/week peak usage. A typical tank size for ammonia distributors is 30,000 gallons. So, with one 30,000 gal tank (installed underground for safety, security and ease of temp/pressure maintenance), we could operate with three a week deliveries from 11,500 gal tank trucks (typical size ammonia trucks). I'm sure the logistics can/will be optimized beyond that, but this will do for illustration.



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1/8 of midwest propane demand and IL annual purchase of NH3 (1 MM tonnes)												
MODEL RESULTS COST, THERMO AND CO2 MATRIX												
USER INPUTS ALLOWED IN GREEN CELLS	ALL VALUES EQUIV 1	ALL VALUES CORRESPOND TO CASE PARAMETERS		AMMONIA NATURAL GAS GASOLINE LPG		LPG	DIESEL	COAL	ETHANOL	METHANOL	DME	
REQUIRED INPUT or CALCULATE Tonnes NH3 for your scenario in D4	1.00	1,000,000		INPUT Price of NH3 delivered to site, S per tonne	INPUT Price of gas delivered to site, \$ / mmbtu	site, \$ / gal	INPUT Price of LPG delivered to site, \$ / gal	INPUT Price of diesel delivered to site, \$ / gal	INPUT Price of coal delivered to site, \$ / tonne	INPUT Price of ethanol delivered to site, \$ / gal	INPUT Price of methanol delivered to site, \$	INPUT Price of DME delivered to site, \$ / tonne
OPTIONAL USER- CERTER VARIABLE. ENTER VARIABLE NAME IN THIS CELL. ENTER (3 T AND BASIS) IN CS. ITERATE D4 TO ACHEVE DESIRED QUANTITY IN D5		0.00		\$350	\$12.00	\$4.00	\$3.50	\$4.00	\$100	\$4.00	\$300	5420
MMBTU (or 1000 CF gas equiv) contained in NH3	21.92	21,318,000		Tonnes NH3 for 21.3 MMBTU	MMBTU gas for 21.3 MMBTU	Gal gasoline for 21.3 MMBTU	Gal UPG for 21.3 MMBTU	Gal diesel for 21.3 MMBTU	Tonnes coal for 21.3 MMBTU	Gal ethanol for 21.3 MMBTU	Tonnes methanol for 21.3 MMBTU	Tonnes DME for 21.3 MMBTU
MMBTU gas required for NH3	\$2.0	32,000,000		14	21.3	177	234	15		25	0.94	6.71
TCF natural gas required for NH3	2346.08	0.029		NH3 Fuel Cost (for 21.3 mmbtu) - This Scenario	Gas Fuel Cost (for 21.3 mmbtu) - This Scenario	Gasoline Fuel Cost (for 21.3 mmbtu) - This Scenario	UPG Fuel Cost (for 21.3 mmbtu) - This Scenario	Diesel Fuel Cast (for 21.3 mmbtu) - This Scenario	Coal Fuel Cost (for 21.3 mmbtu) - This Scenario	Ethanol Fuel Cost (for 21.3 mmbtu) - This Scenario	Methanol Fuel Cost (for 21.3 mmbtu) - This Scenario	DME Fuel Cost (for 21.3 mmbtu) - This Scenario
Tonnes water produced from NH3	1.586-00	1,580,000		\$350	\$256	5688	5819	\$624	\$104	\$1,013	\$294	\$298
# Global ammonia industry	6.676-09	0.007		kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 like)	(kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 like)	kwh from 21.3 mmbtu at 35% efficiency (coal like)	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 like)	kwh from 21.3 mmbtu at 35% efficiency (coal like)	kwh from 21.3 mmbtu at 35N efficiency (coal like)	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3 8ke)	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3	kwh from 21.3 mmbtu at 45% efficiency (gas/nh3
# of World Scale NH3 Plants	1296-06	1.25		2600	2800	2200	2800	2200	220	280	280	2800
Number of 60,000 dam vessels	2446-05	24		Fuel cost for power, \$/kwh from NH3	Fuel cost for power for power, 5/kwh from gas	Fuel cost for power, \$/kwh from gasoline	Fuel cost for power, S/kwh from LPG	Fuel cost for power, \$/kwh from diese!	Fuel cost for power, \$/kwh from coal	Fuel cast for power, S/kwh from coal	S/kwh from methanol	Fuel cast for power, S/kwh from DME
Number of 80 tonne raikar deliveries	6.0125	12,500		\$0.125	\$0.091	\$0.313	\$0.293	\$0.284	\$0.047	\$0.363	\$0.105	\$0.107
# of 1 MM TPA NH3 pipeline	1.005-06	1.0	AMMONIA, NO CCS	AMMONIA w/ HARVEST	NATURAL GAS	GASOLINE T CO2 per 23-3 mmbro	LPG	DIESEL T CO2 per 23-3 mentes	COAL	ETHANOL T CO2 per 21.3 mmbm	METHANOL	DME T CO2 per 21.3
MWh from 45% efficient power plants	2.812-00	2,810,000	membru, only production, no CCS	membru, only production, CO2 harvest	NOT COUNTING UPECYCLE	NOT COUNTING UPECYCLE	NOT COUNTING UPECYCLE	NOT COUNTING UFECYCLE	NOT COUNTING UFECYCLE	NOT COUNTING UFECYCLE	COUNTING LIFECYCLE	counting LIFECYCLE
e of 20 MW plants that can be run for 1 year, 45%	3.218-05	32.1	1.93	0.68	1.23	1.65	1.48	1.68	2.42	0.33	1.80	1.80
Equivalent # of 6 mtpa LNG train (8TU basis)	6.872-08	0.07	Midurat	Contilizer 11-	at and Ele	CASE	NOTES					
Tonnes UNG equivalent	0.41	410,000	wiidwest	Fertilizer, He	eat and Elect	ricity						
Metric Tonnes coal equiv	1.54	1,040,000	The Midwest	tern states ran o	dangerously lov g availability of	v of LPG for hea	at and farm use	this winter with	h emergency m	easures		
(106)	6.500	500,000	of propane v	was strained by	high demand fo	or drying extra v	wet crops follow	ved by record c	old.	ry and storage		
Tonnes resid equiv	0.530	530,000	Prices rose to	o \$4-5 per gallo	n (normally aro	und \$2). And a	lot of people g	ot really cold a	nd mad.			
Gal LPG equiv	254	234,000,000										
Gal Gasoline equiv	172	172,000,000	l've modelle ammonia fe	d ammonia equ rtilizer), If 12.5	ivalent to 12.5% % of LPG dema	6 of Midwest p od were stored	ropane demand at ammonia fac	l (also equivale ilities at the en	nt to Illinois der d of harvesting	mand for and the start	l	
Gal Ethanol equiv	253	253,000,000	of winter (w	hen these facili ubstantial cushi	ties are operati	ng low because g the costs and	they are most risks of LPG sh	full before and ortages. This is	during planting	season), this 30 MM gal		
Total NH3 cost \$		350,000,000	LPG (replace equivalent B	ed by 1 MM ton STUs of LPG at \$	nes ammonia). 2/gal is \$468 M	The total cost IM and at \$4/ga	of that ammoni al is \$936 MM.	a at \$350/tonn There clearly is	e is \$350 MM. large financial	The cost of the incentive even		
Fuel cost for power, S/kuch form MET	5 0.125		without the	consideration o	of risk managem	ient.		, .	6-			
Price NATURAL GAS	\$12.00		If Sturman e	engine 1.0 MW	units (40' trailer	s with Sturman	fitted control s	ystems) were s	ited on farms a	nd		
Total Natural Gas cost \$		\$ 255,600,000	units are als	o ideally suited	for CHP (total e	fficiency up to	75% or so) which	th can be used	for district heat	ing and, very		
Fuel cost for power for power, S/kwh from gas	\$ 0.091		importantly,	, crop drying.								
Price GASOLINE	54.00		One other h winter and s	uge advantage pring (for plant	is countercyclic ing) and the LP	al infrastructur G infrastructure	e use. The amn e is weighted to	nonia infrastruc ward summer a	ture is weighte and fall (for cro	d toward p drying and		
Total Gasoline cost \$		\$ 688,000,000	winter heati	ing). The ammo	onia producers v	will be happy to	have profitable	e smoothing of	their storage ar	nd distribution.		
Fuel cost for power, S/kwh from gasoline	5 0.313											
Price UPG	\$3.50											
Total LPG cost S		\$ 819,000,000										
Fuel cost for power, \$/kwh from LPG	\$ 0.293											
Price DIESEL	\$4.00											
Yotal Diesel cost \$		\$ 624,000,000										
Fuel cost for power, S/kwh from diesel	\$ 0.284											
Price COAL	\$100											
Total Coal cost \$		\$ 104,000,000										
\$/kwh from coal	\$ 0.047											
Price ETHANOL	54.00											
Total Ethanol cost 5		\$ 1,012,000,000										
S/kwh from ethanol	5 0.361										1	

#### MidWest LPG Demand

The Midwestern states ran dangerously low of LPG for heat and farm use this winter with emergency measures required. Even with growing availability of propane from shale oil and gas, the infrastructure for delivery and storage of propane was strained by high demand for drying extra wet crops followed by record cold.

Prices rose to \$4-5 per gallon (normally around \$2). And a lot of people got really cold and mad.

1/8 of MidWest LPG demand is 1 MM TPA NH3. Even at \$500 per tonne, ammonia BTUs are 20% cheaper than \$4/gal LPG.

If ammonia diesel gens were sited on farms and neighborhoods, they would produce well-conditioned power for local use and utility offtake at 45% efficiency. The units are also ideally suited for CHP (total efficiency up to 75% or so) which can be used for district heating and, very importantly, crop drying.

One other huge advantage is countercyclical infrastructure use. The ammonia infrastructure is weighted toward winter and spring (for planting) and the LPG infrastructure is weighted toward summer and fall (for crop drying and winter heating). The ammonia producers might be happy to have profitable smoothing of their storage and distribution.



