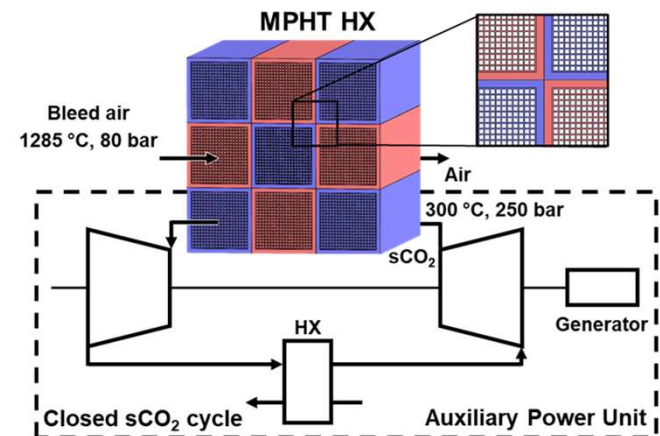


Multiscale Porous High-Temperature Heat Exchanger Using Ceramic Co-Extrusion

Evelyn N. Wang, MIT

We are developing a novel high performance, compact and durable ceramic heat exchanger design with a multi-scale porous configuration by scalable co-extrusion fabrication for aerospace applications.



Brief Project Overview

Fed. funding:	\$1.7M
Length	36 mo.

Team member	Location	Role in project
MIT	Cambridge, MA	Design, modeling and characterization
Purdue University	West Lafayette, IN	Fabrication and mechanical characterization
General Electric	Niskayuna, NY	High temperature demonstration and commercialization

Context/history of the project

- MIT: Multi-scale porous heat exchanger design with compact headers
- Purdue: Ceramic co-extrusion fabrication to enable the design
- GE: High-temperature demonstration and commercialization of heat exchangers

- Goal: Design, fabricate and characterize a high-performance multiscale ceramic HX with scalable co-extrusion method

Brief Project Overview

Fed. funding:	\$1.7M
Length	36 mo.

MIT

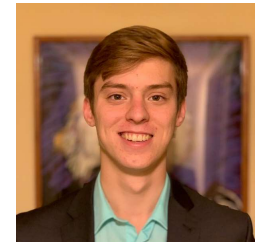
- PI: Evelyn Wang
- Postdoc: Xiangyu Li
- Graduate Student: Chad Wilson



Evelyn N. Wang



Xiangyu Li



Chad Wilson

Purdue

- co-I: Rodney Trice, Jeffrey Youngblood
- Graduate Student: Rodrigo Orta Guerra, Olivia Brandt



Rodney Trice



Jeffrey Youngblood

GE

- co-I: Gregory Natsui
- Eyitayo Owoeye



Gregory Natsui



Eyitayo Owoeye



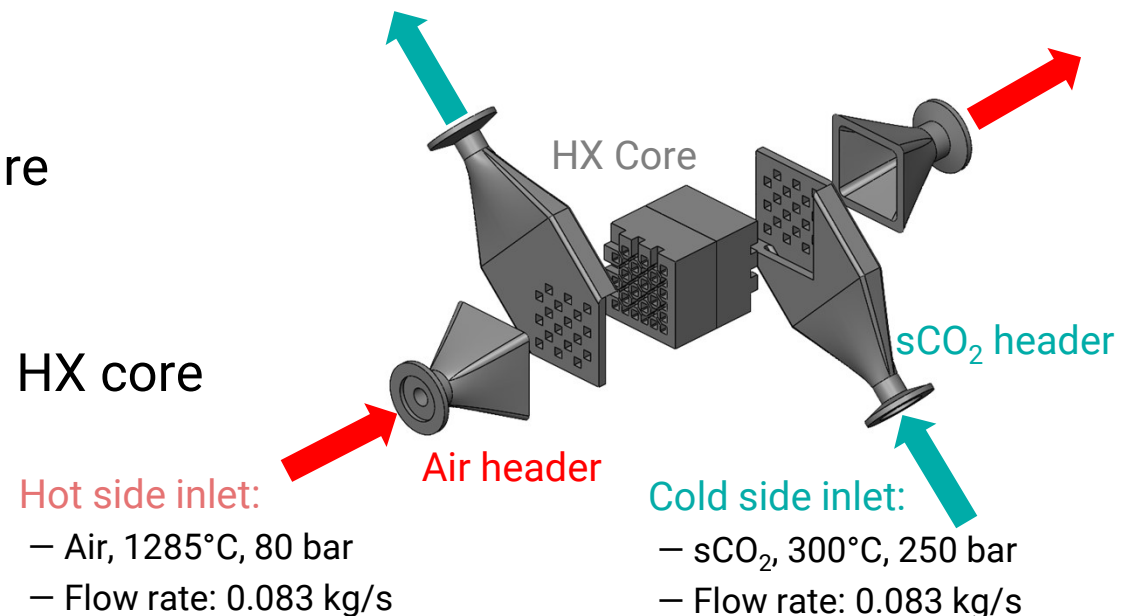
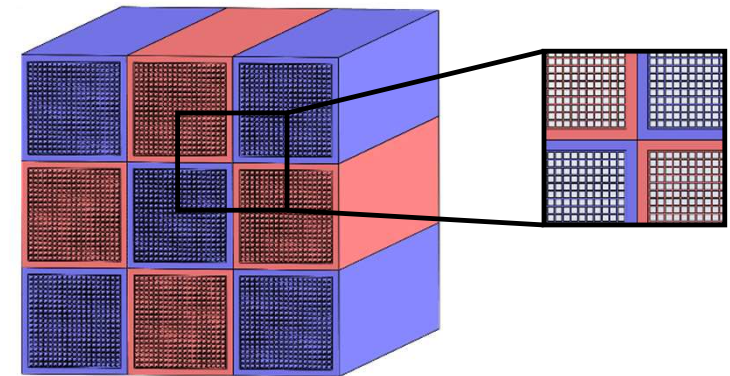
Rodrigo Orta Guerra



Olivia Brandt

Heat Exchanger (HX) Design Details

- ▶ Multiscale porous counterflow design
 - Enhanced performance
 - Low pressure drop
- ▶ Ceramic co-extrusion fabrication
 - Scalable and low cost
 - High temperature and pressure
- ▶ Compact header integration with HX core



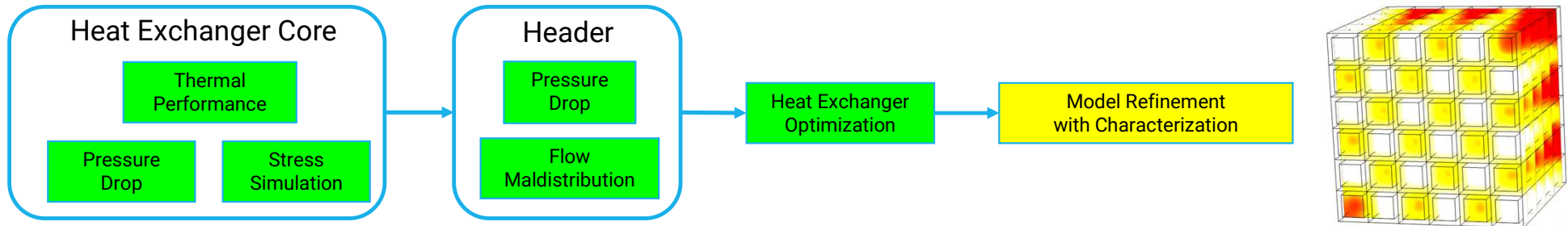
Heat Exchanger Design Details

Metric Name	Category B Target	MPHT HX Core Performance
Targeted application(s)		Aviation
Hot-side pressure drop, $(\Delta P/P_{inlet})_{hot}$	$\leq 4\%$	$\leq 4\%$
Cold-side pressure drop, $(\Delta P/P_{inlet})_{cold}$	$\leq 4\%$	$\leq 4\%$
Heat exchanger effectiveness	$\geq 50\%$	$> 50\%$
Heat exchanger thermal capacity	$\geq 50 \text{ kW}_{th}$	50 kW_{th}
Heat exchanger mass-based power density	kW_{th}/kg	$> 100 \text{ kW}_{th}/\text{kg}$
Heat exchanger volume-based power density	$\text{kW}_{th}/\text{m}^3$	$> 7 \times 10^5 \text{ kW}_{th}/\text{m}^3$
Heat exchanger material(s)		SiC

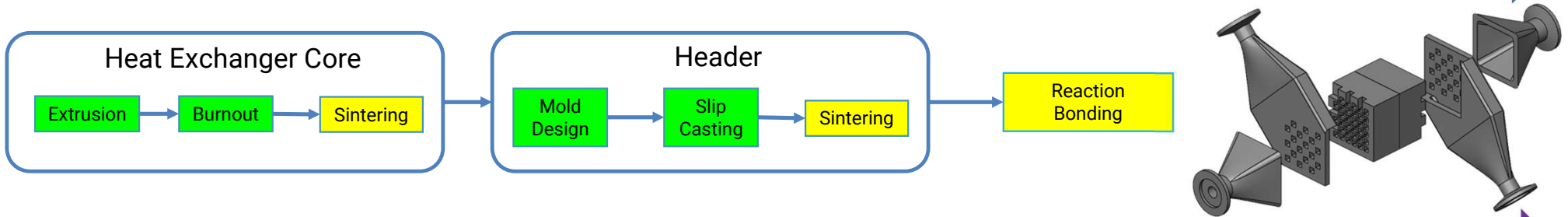
- ▶ Detailed multiscale model of the heat exchanger core
- ▶ A HX core predicted with $> 50\%$ effectiveness and $> 700 \text{ MW}_{th}/\text{m}^3$, $> 100 \text{ kW}_{th}/\text{kg}$ power density

Progress Against Tasks – Timetable

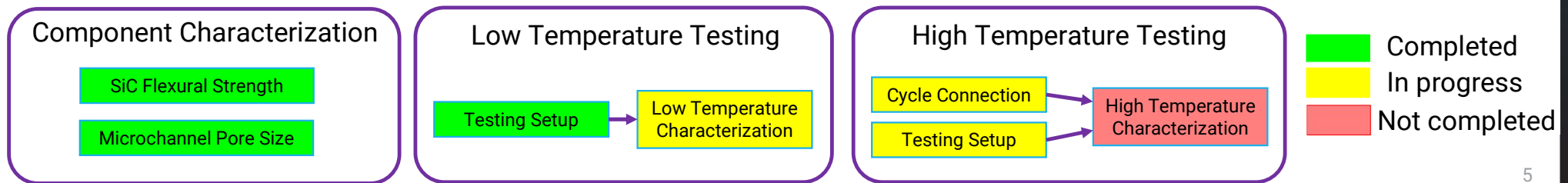
Modeling and Optimization



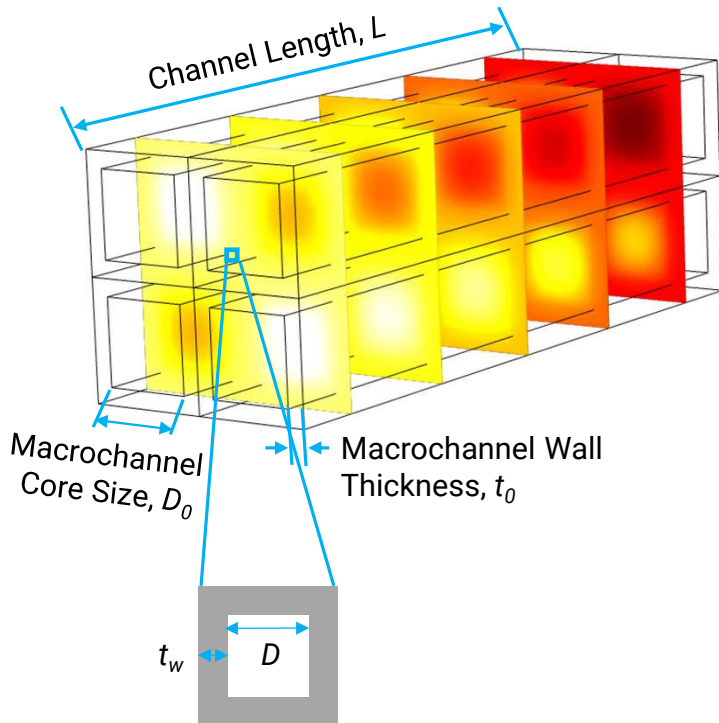
Heat Exchanger Fabrication



Testing and Characterization



Model Overview of the Heat Exchanger Core

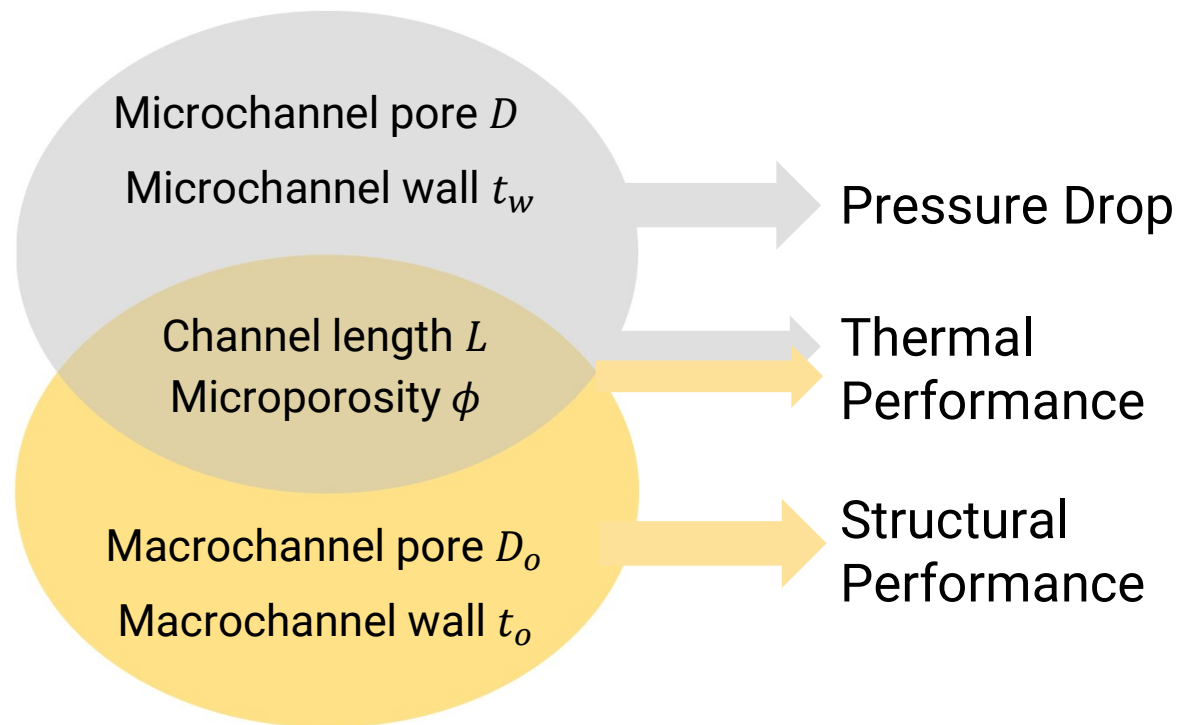


Microchannel Dimension

$$\text{Microporosity } \phi = \left(\frac{D}{D+2t_w} \right)^2$$

Design Parameters

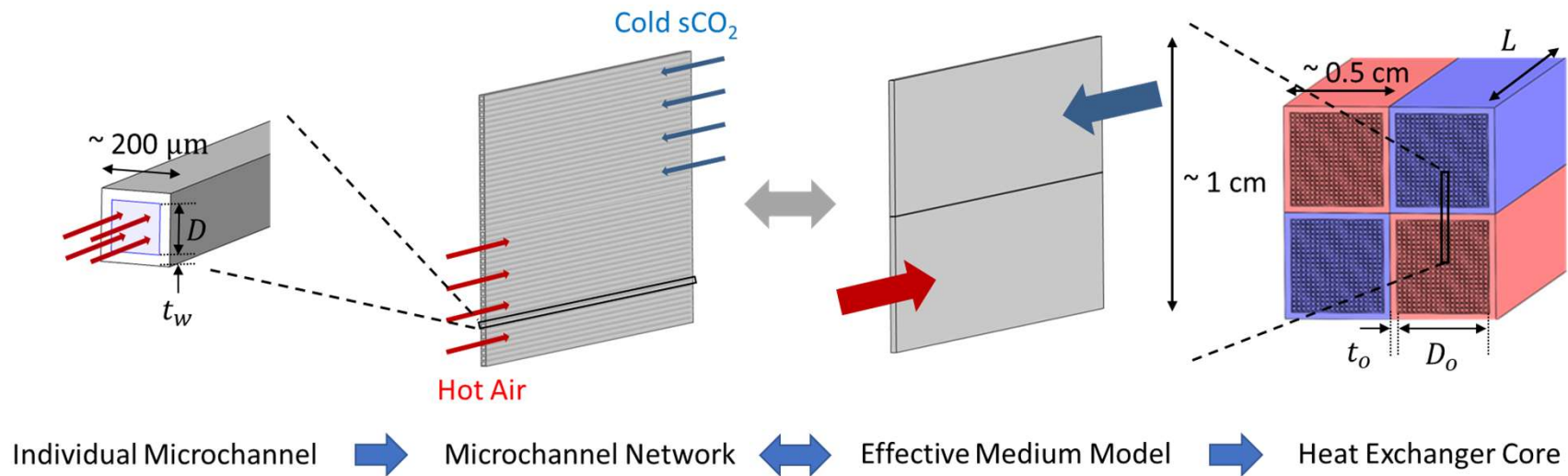
Performance Metrics



Thermal-Fluidic Modeling

► COMSOL Hierarchical Thermal-Fluidic Simulation

- Fluidic simulation in individual microchannels for pressure drop
- Effective thermal conductivity for microchannel network
- Optimizing HX core for thermal performance



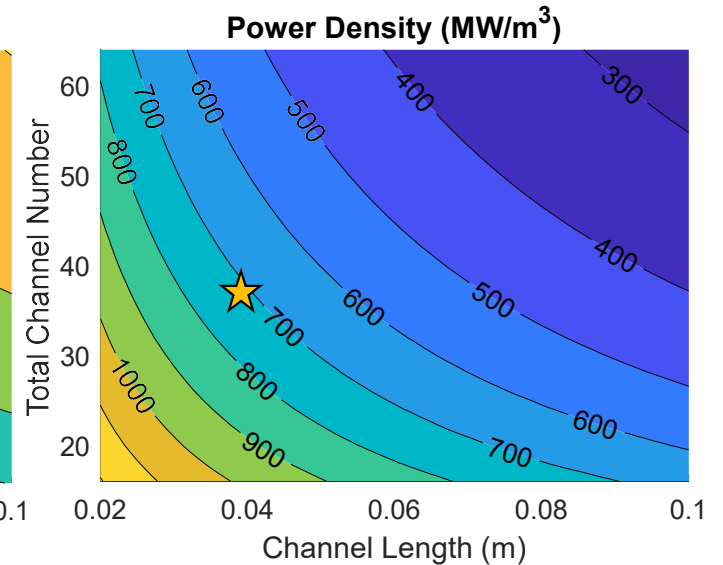
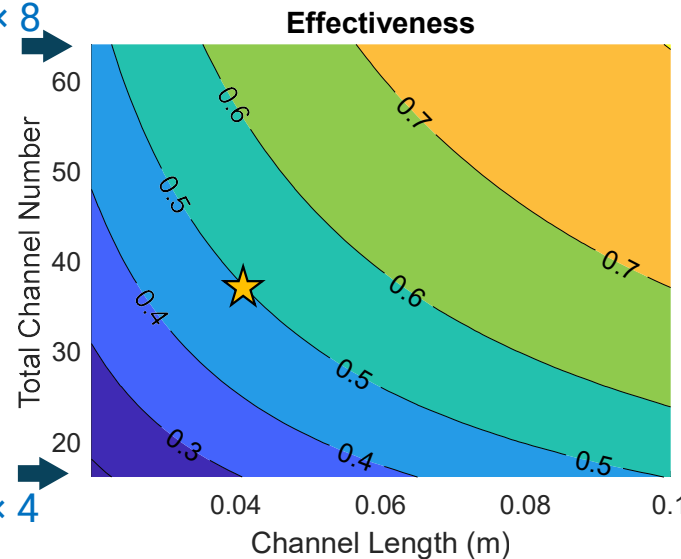
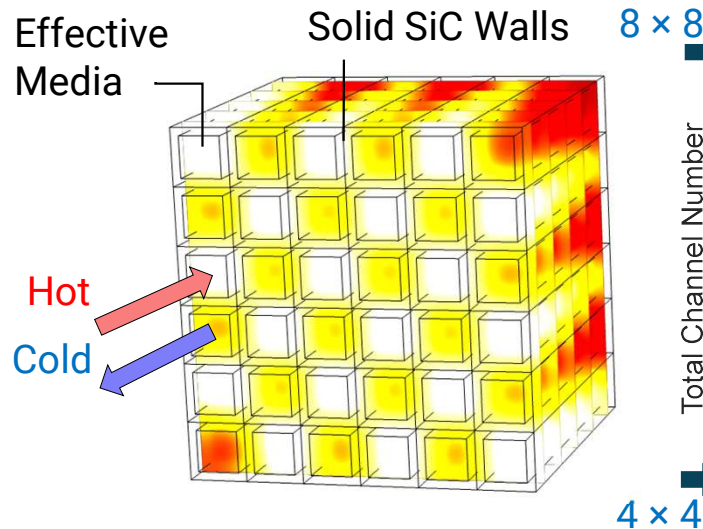
HX Prototype Optimization

► 0.083 kg/s mass flow rates

Geometry Parameters	Current Design
Microporosity, ϕ	0.34
Microchannel Size, D	105 μm
Channel Length, L	4 cm
Macrochannel Size, D_o	5 mm
Macrochannel Wall, t_o	1 mm

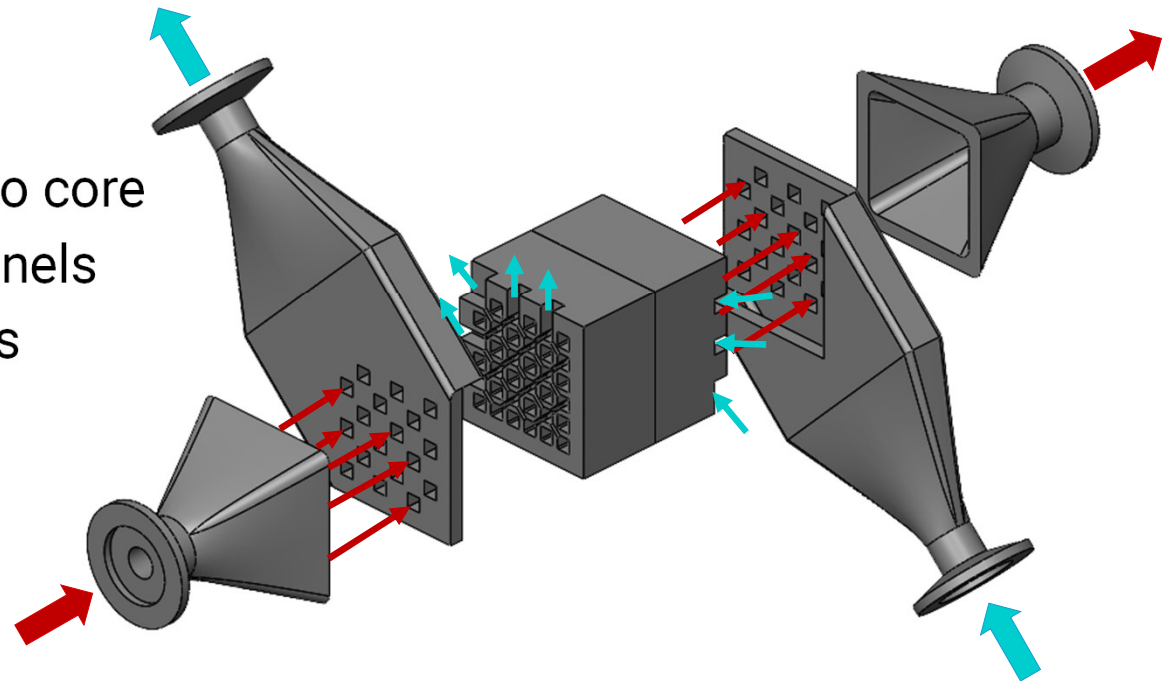
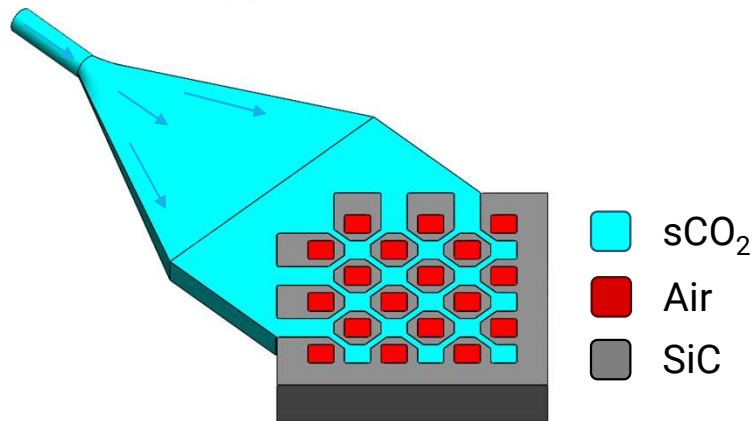
► HX Core Performance

- Heat Capacity, 51 kW_{th}
- Pressure Drop, $\Delta P/P < 2\%$
- Effectiveness, $\varepsilon > 50\%$
- Volume Power Density, 700 MW/m³
- Weight Power Density, 230 kW/kg



Header Design

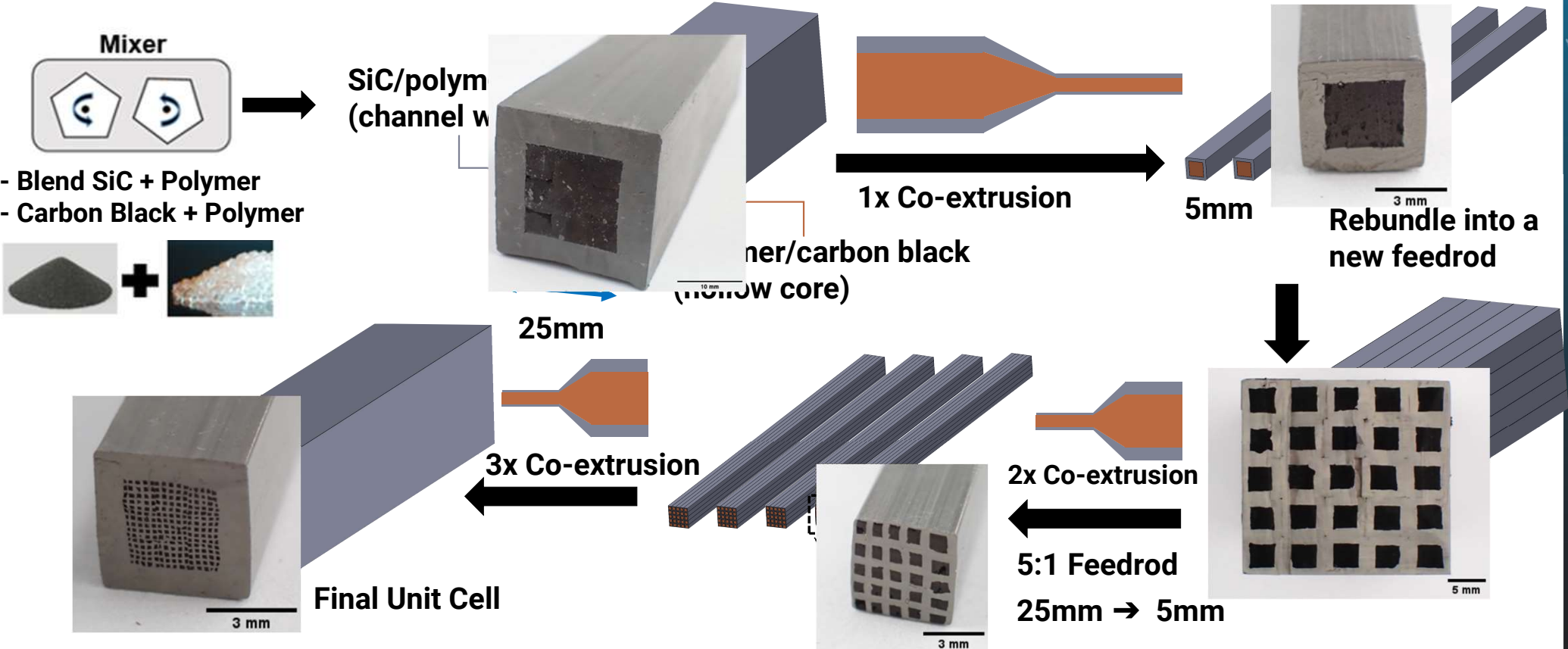
- ▶ Goal: Low pressure drop without sacrificing manufacturability
- ▶ Solutions:
 - Mill part of header directly into core
 - Air inlet in line with core channels
 - sCO₂ inlet turns 90° in headers



- Total pressure drop: $\Delta P/P < 4\%$
- Flow maldistribution: 1.4 g/s

* Model refinement ongoing with experimental characterization

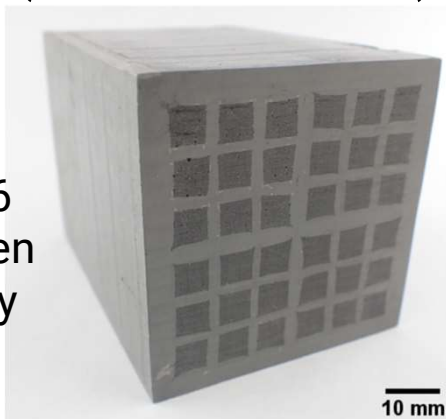
Co-Extrusion of Microchannels - Manufacturing Process Overview



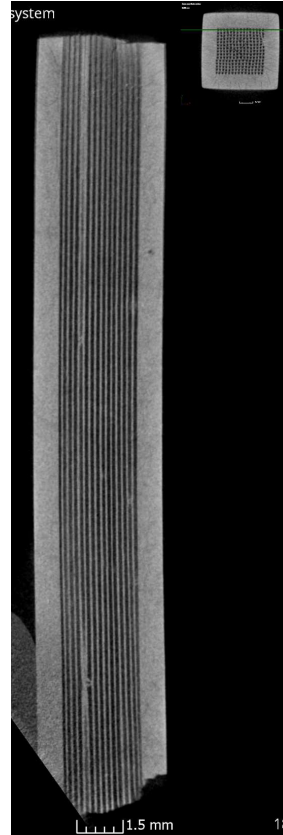
Scale Up of Heat Exchanger and Microchannel Openness

- ▶ Finalized 6 by 6 heat exchanger design
 - Each unit cell has 625 square microchannels, approx. $100\ \mu\text{m} \times 100\ \mu\text{m}$ (22,500 channels)

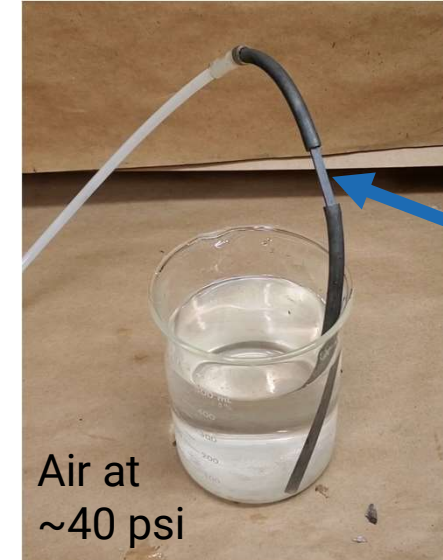
6 x 6
Green
Body



- ▶ Microchannels are open and continuous after sintering



microCT of unit cell after sintering (courtesy APL/JHU)

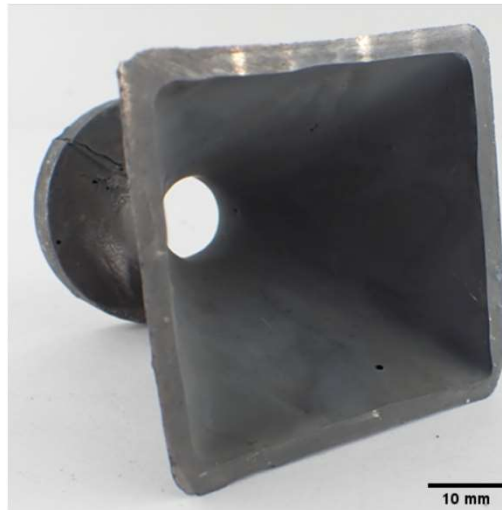


25 mm
long
sintered
SiC
unit
cell

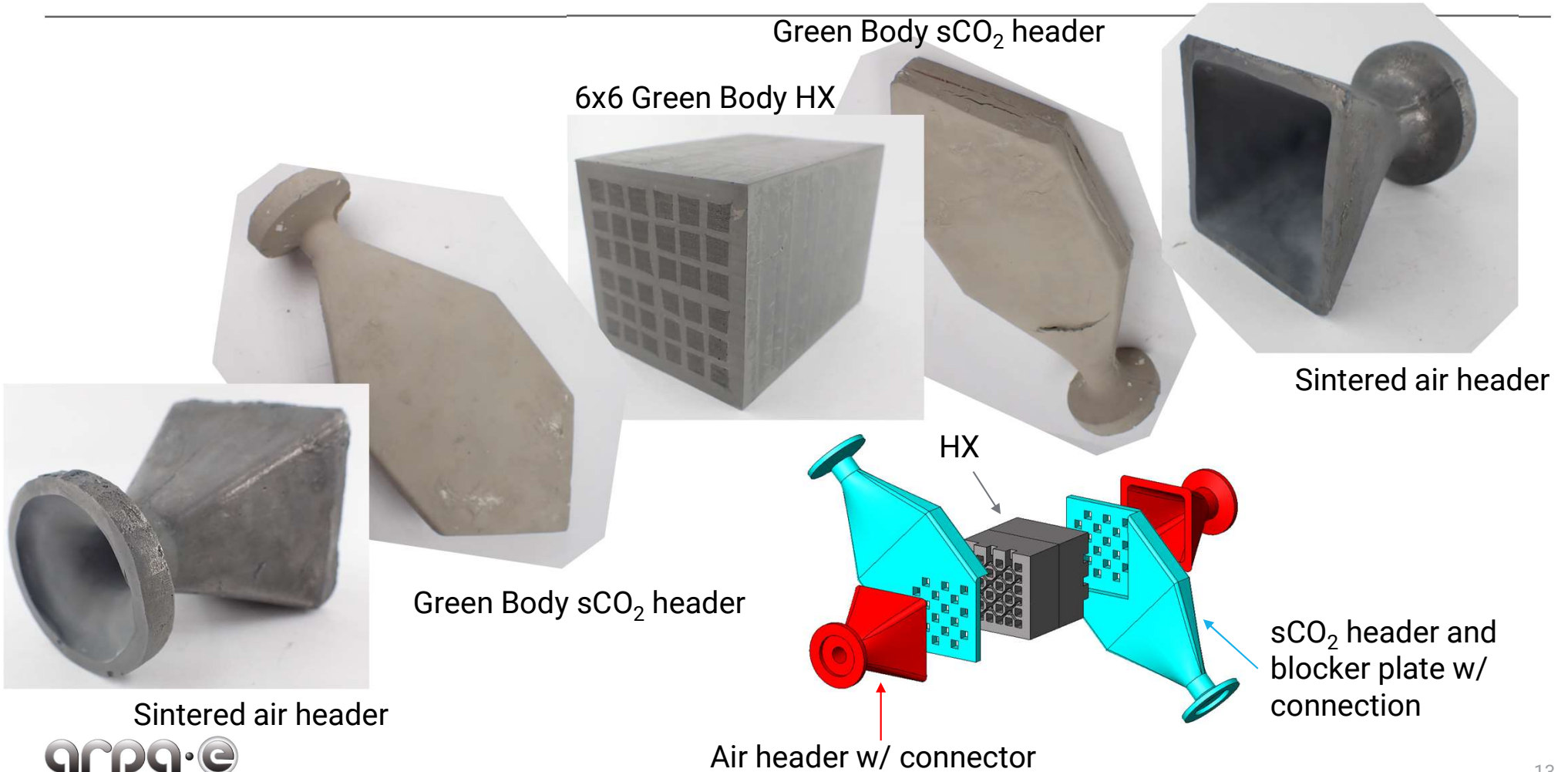
Slip Casting of SiC for Header Fabrication

- ▶ Fabrication of air and sCO₂ headers through SiC slip casting
- ▶ Successful sintering of air header with 96% RD
- ▶ Parts complete and ready for bonding

Slip cast SiC part

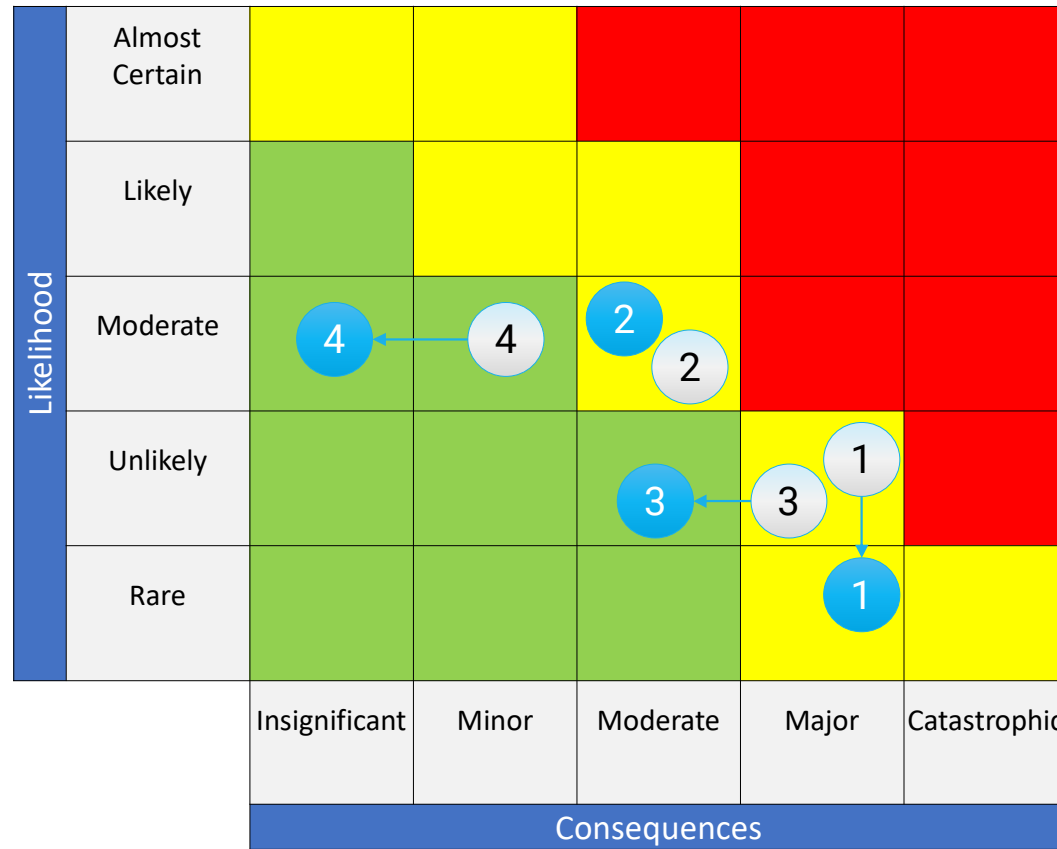


Fabrication of Heat Exchanger and Headers Progress



Risk Update

Risk	#
Unsuccessful co-extrusion of SiC	1
Weak joint between SiC components	2
Poor durability of the heat exchanger	3
Not ideal for aircraft APUs	4



- X Now
- X Start of project

Technology-to-Market Updates

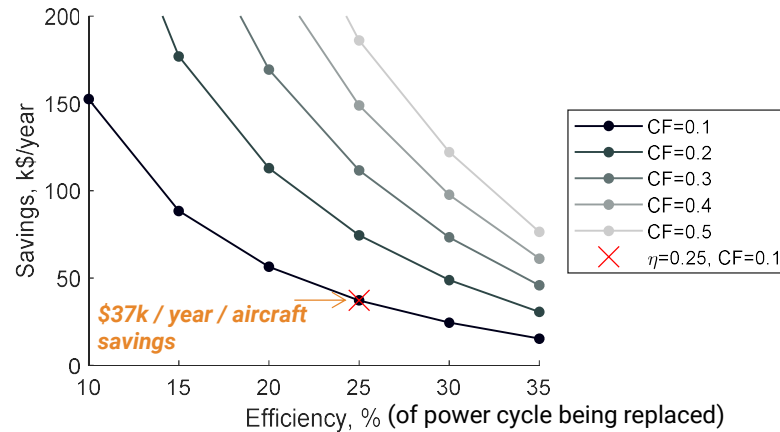
▶ Notable accomplishments

- System level value proposition
- Initial market surveys
- Initial monetization plan
- IP study complete, HX core design has been filed as a disclosure
- Characterized first markets
- Drop-in value propositions
- Costing model

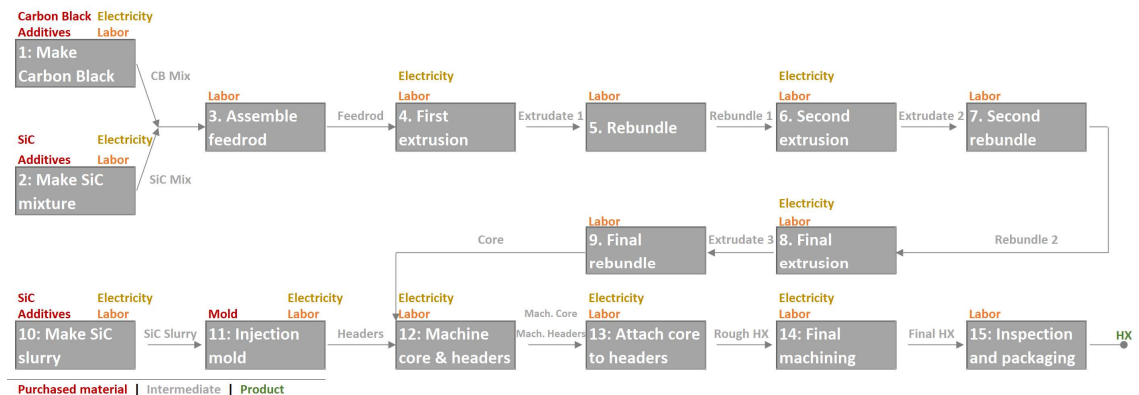
▶ Key assumptions driving economic viability

- Willingness to adopt
- Targeting low-risk first markets

Value proposition of a new power cycle in aircraft APU



Cost model process diagram



Potential Partnerships

- ▶ Needs at this time
 - Industrial co-extrusion entity
 - **Applications**
 - **Immediate (drop-in): may not leverage full capabilities – but – ideal first market**
 - Long term (advanced system): yield greater value stories – but – not ideal near term
 - Identify a follow-on program which utilizes our technology in a system.

Q & A

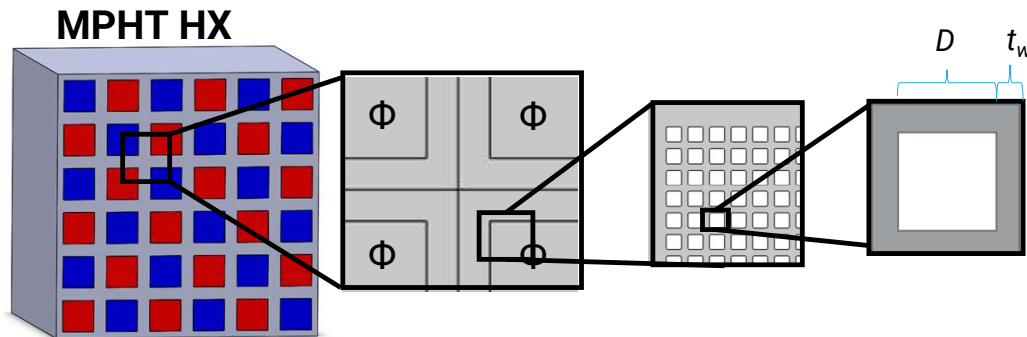


U.S. DEPARTMENT OF
ENERGY

<https://arpa-e.energy.gov>

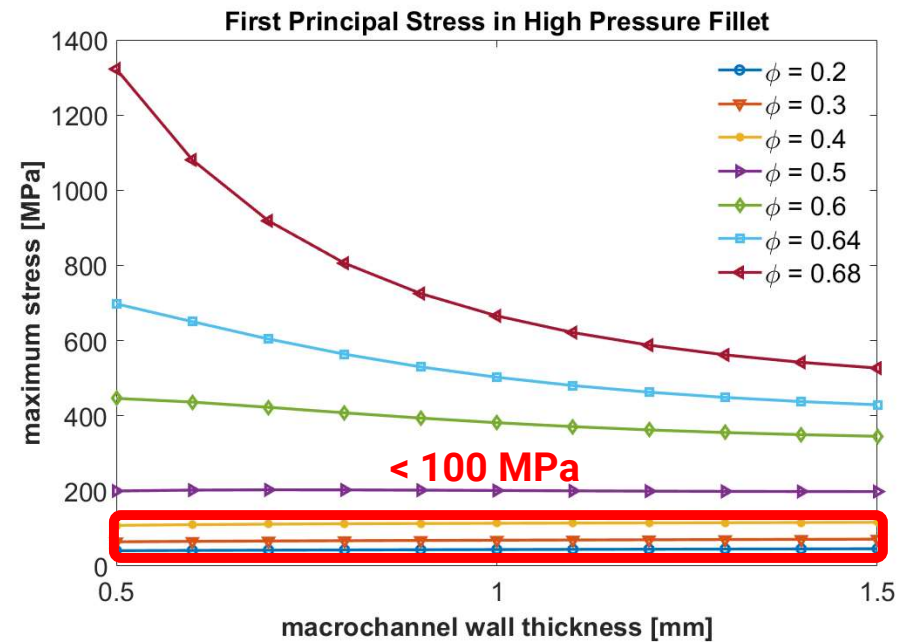
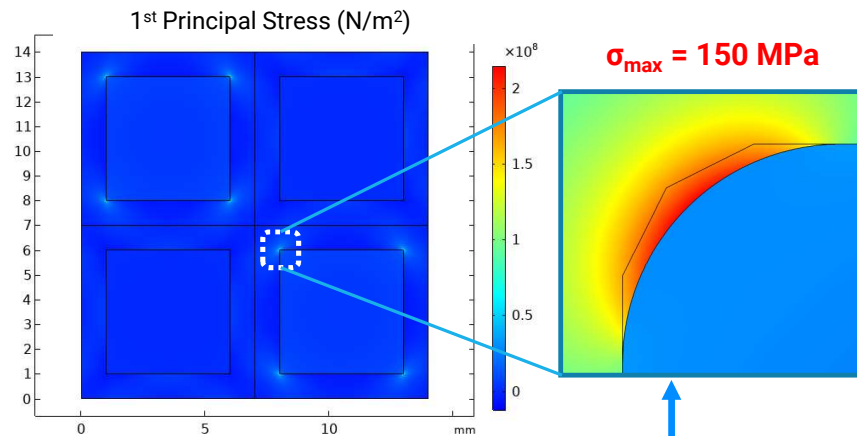
Structural Performance of HX Core

Microscale geometry adjustment



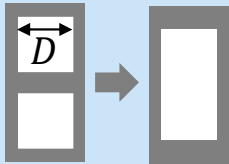
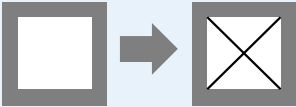
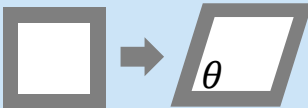
Current: $D = 105 \mu\text{m}$, $t_w = 38 \mu\text{m}$

$\Phi_{\text{original}} = 50\% \rightarrow \Phi_{\text{actual}} = 34\%$

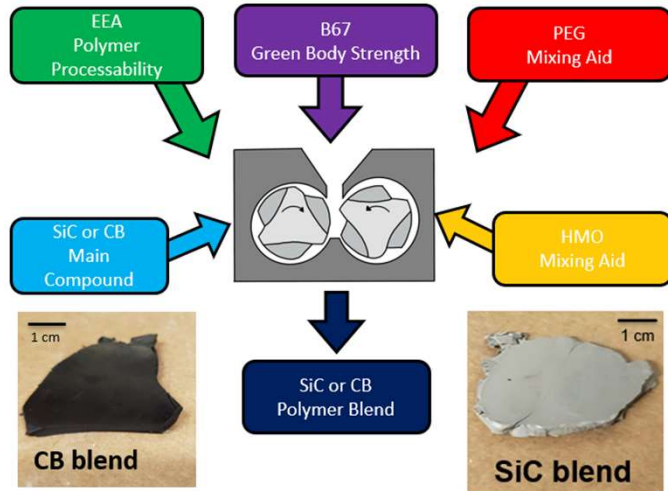


$$E_{\text{porous}} = (1 - \phi) \frac{1 - \phi}{0.684} E_{\text{sic}}$$

Summary – Imperfect Square Channels

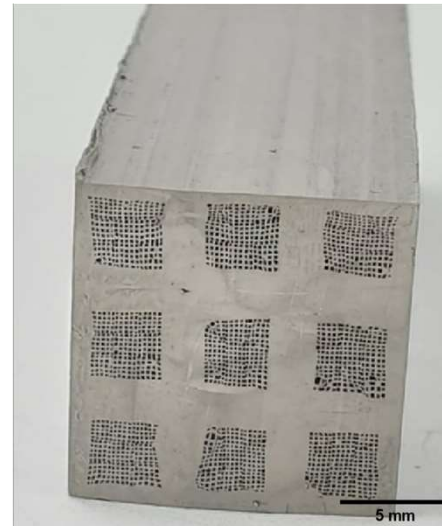
Microchannel Imperfection	Percentage/ Likelihood	Effect on pressure drop	Effect on power density	Effect on mechanical strength
Merged channels 	< 5%	Minor reduction	Minor reduction	No significant impact
Blocked channels 	< 5%	Minor increase	Minor reduction	Minor enhancement
Rhombus channels 	< 5%, 60°-90°	Minor increase	Minor enhancement	No significant impact

Silicon Carbide 3 by 3 Heat Exchanger Fabrication

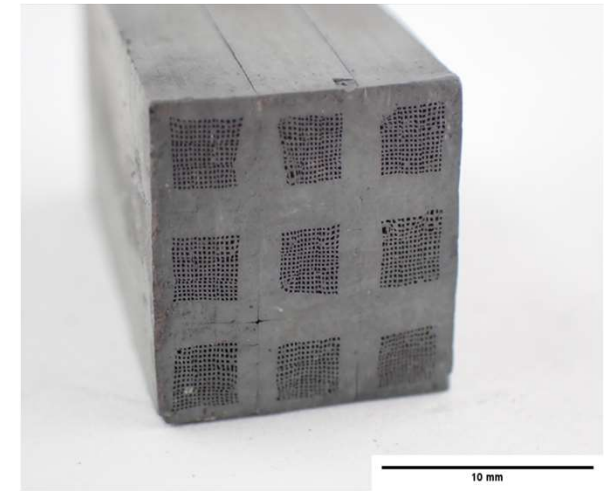


Vol% SiC or Carbon Black	Torque (N-m)	Temp (°C)
54 vol% SiC*	16.5	149
40 vol% CB	17.1	147

* SiC plus sintering aids ($Al_2O_3 + Y_2O_3$)



Green body 3 x 3 prototype



Sintered 3 x 3 prototype

- Torque matching of blends for co-extrusion
- Removal of polymer without distortion
- Sintering of SiC to 90% Relative Density