

# R&D Opportunities in Head-end Processing and Off-gas Management

Stephanie Bruffey

R&D Staff

Oak Ridge National Laboratory

*Presented at ARPA-E CURIE Workshop*

*July 28<sup>th</sup>, 2021*

ORNL is managed by UT-Battelle LLC for the US Department of Energy

# Outline

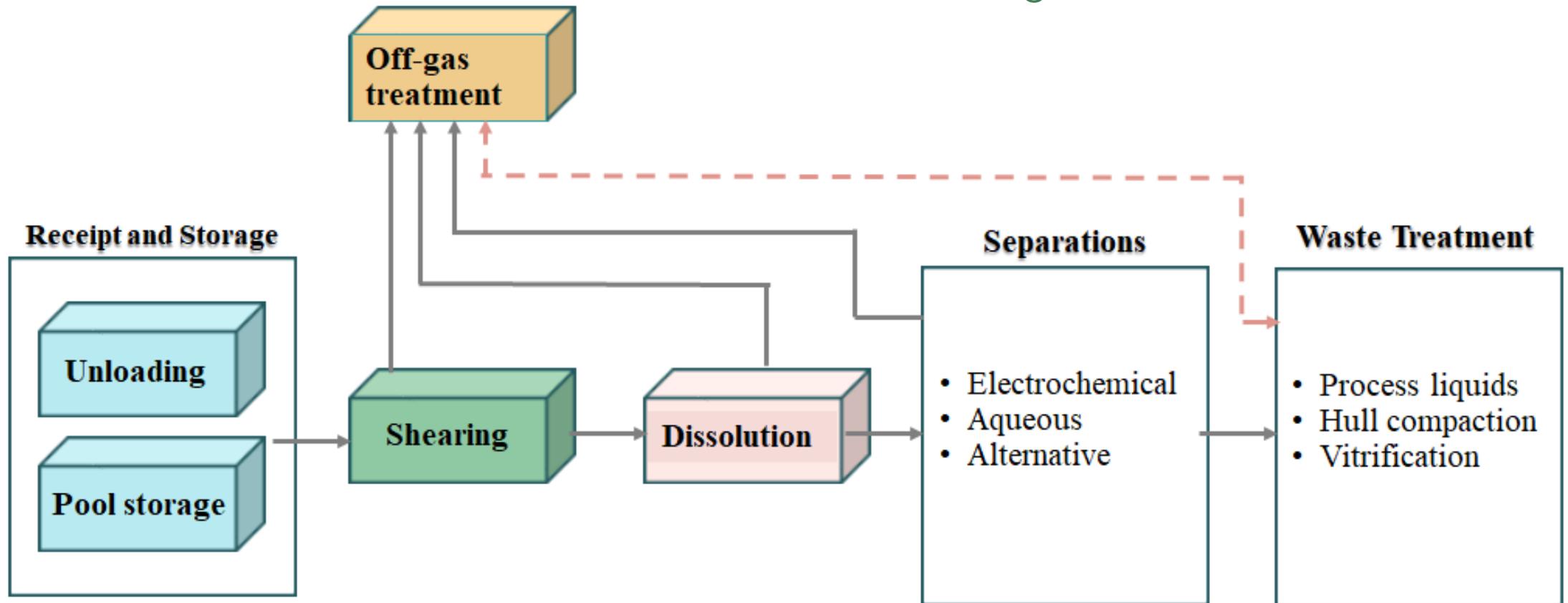
- What is head-end processing and off-gas management?
- Why are we interested in these aspects of fuel processing?
- How do these processes work within a facility?
- Where are there opportunities for improvement?

**Head-end:** handling of fuel assemblies prior to beginning chemical separations.

- Pool storage
- Disassembly or hardware removal
- Shearing/Fuel meat exposure

**Off-gas:** All gaseous process streams within a facility requiring treatment.

- Contains volatile fission products, including noble gases
- Radioactive emissions must be managed to comply with regulatory discharge limits



# Access to cost information can be challenging, but we do know the following:

- **Shielded hot cells** are required for handling spent fuel until activity is reduced through chemical separations
- **Fuel assemblies for Gen III+ reactors are long**
  - *Westinghouse 17X17  $\geq$  12 feet active fuel length*
  - *PWR assembly length > BWR assembly length*
- The head-end portion of the plant is typically **less flexible**, relies on mechanical operations, and can be a limiter in terms of **operational availability**
- Requires **remote maintenance**

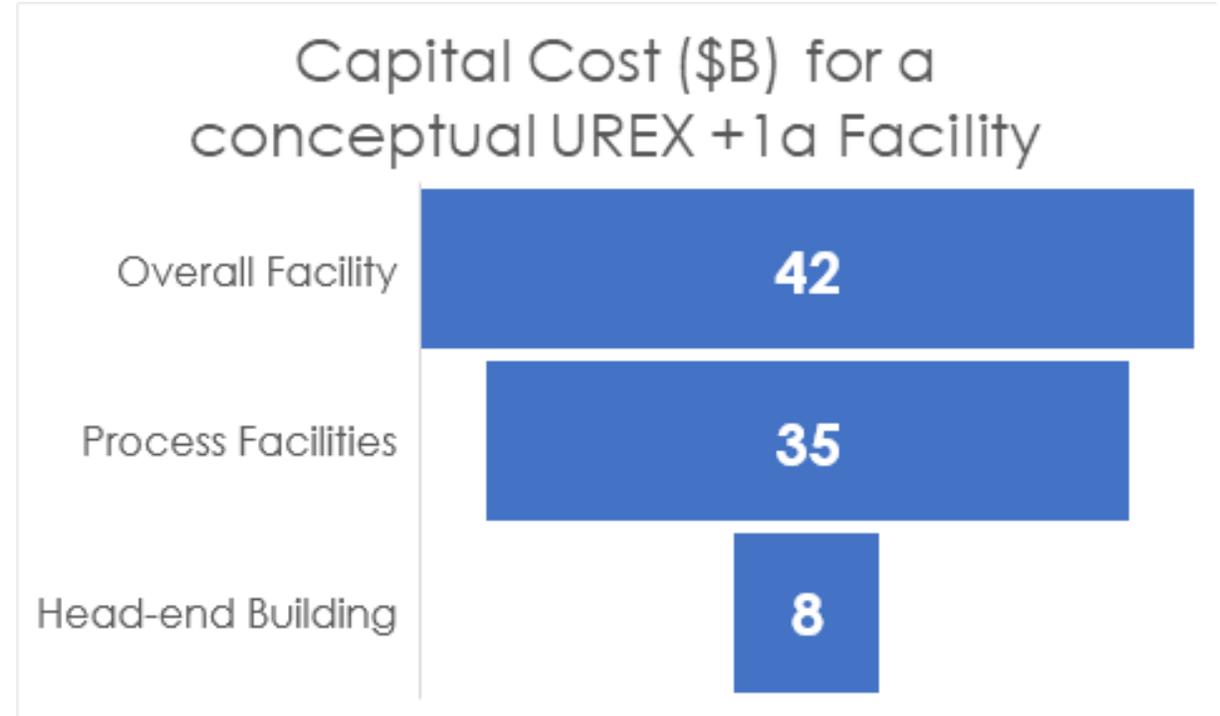
# Consider a conceptual UREX +1A plant:

## Plant specifications:

- UREX +1a separations design
- 3000 MT/y throughput

## Head-end building contained:

- Fuel receipt
- Fuel storage (SFP)
- Fuel shear
- Fuel dissolution
- Dissolver off-gas treatment
- Hulls rinse/compaction
- Tc management



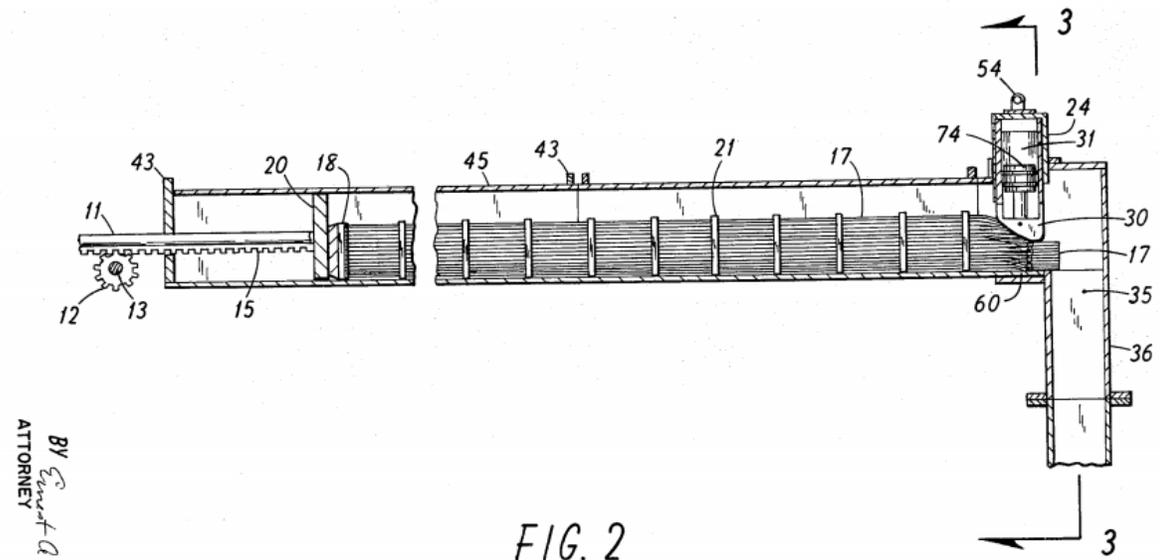
Dixon, et al. *Advanced Fuel Cycle Cost Basis – 2017 Edition*. NTRD-FCO-2017-000265. September 2017.

# Things that decrease capital cost can also reduce operating and maintenance costs.

- Decrease capital through:
  - Decrease of overall facility footprint, but especially shielded space
  - Improved equipment design and fabrication
- Decrease shielded footprint:
  - Early volume reduction
  - Early decontamination to glovebox-acceptable activity levels
  - Choose equipment with small footprints, choose flowsheets with fewer, smaller, and less shielded operations
- Large physical footprints *for aqueous*:
  - Mechanical shear
  - Dissolver off-gas treatment
  - FP/HLW waste treatment and associated off-gas

# What's the baseline for head-end processing?

- **Fuel receipt**
- **Fuel storage** – available wet storage can vary widely across designs and is important in costing the head-end
- **Shearing of  $UO_x$  fuel**
  - Many types of shear designs
    - Bundle shear, single pin shear
  - Alternative blade designs
  - Shearing disadvantages:
    - Creates dust
    - Releases fission products
    - Causes segment crimping



BY *Ernest A. Pavin*  
ATTORNEY  
INVENTORS  
CHESTER S. EHRLMAN  
LOUIS SCHEIB  
CHARLES S. WORSLEY  
FRANK J. JONES  
ROBERT M. FREEBORG

FIG. 2

PATENTED OCT 9 1973

SHEET 2 OF 7

3,763,770

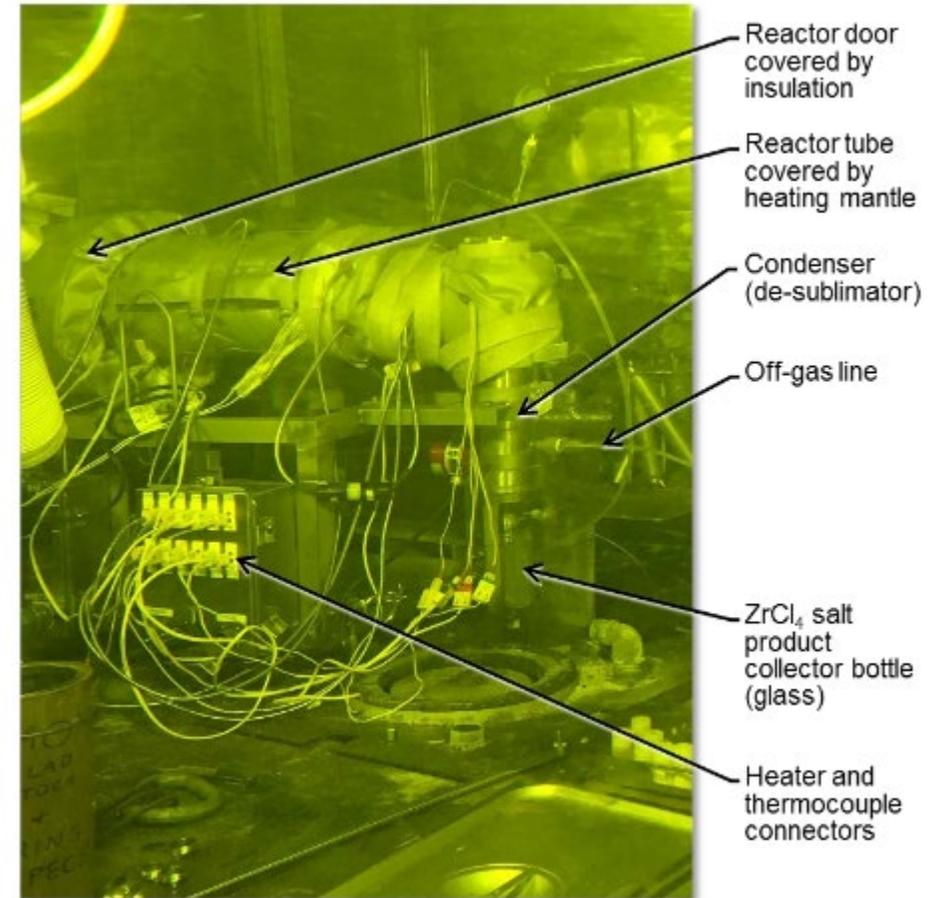
Worsley, C., Jones, F., Ehrman, C., Scheib, L., & Freeborg, R. (1973). U.S. Patent No. 3,763,770. Washington, DC: U.S. Patent and Trademark Office.

Gullwings  
Guillotines  
Dogbones?

# Alternative to Shearing: Chemical decladding

- Chlorination, hydrochlorination
- Electrolytic removal of zirconium
- Sulfur chlorination digestion
- Dissolution in  $\text{NH}_4\text{F}$  (ZIRFLEX)

➤ Product should eventually be  $\text{ZrO}_2$  if disposal is desired. The nuclear grade zirconium is valuable if highly pure and if end-users will tolerate Zr-93 ( $t_{1/2} = 1.56 \times 10^6$  y).



**Chlorination of 0.5 kg of irradiated hulls in ORNL Hot Fuel Examination Facility**

# Questions around chemical decladding...

- What does the reaction vessel look like?
- Is disassembly required?
- Is shearing required?
- Is the uranium-bearing product compatible with downstream processing?
- How does this impact the hulls processing baseline?

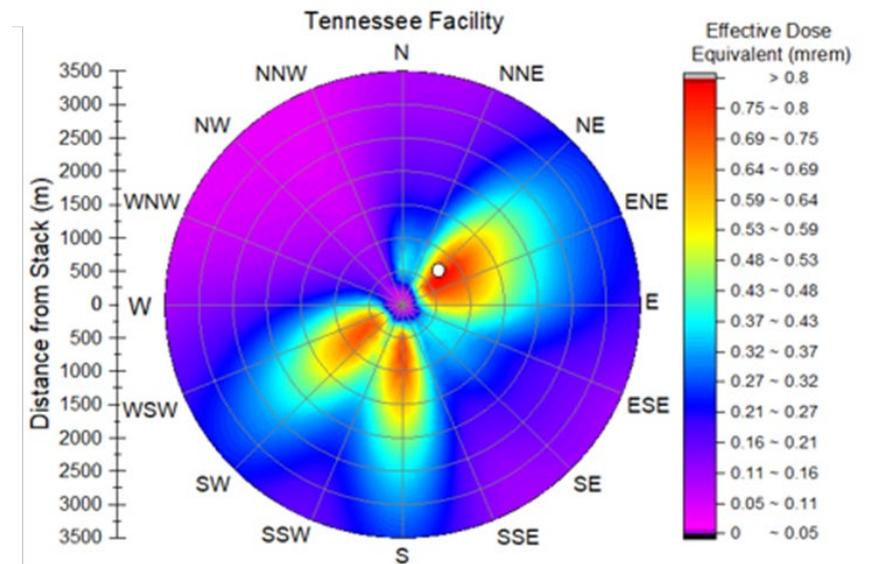
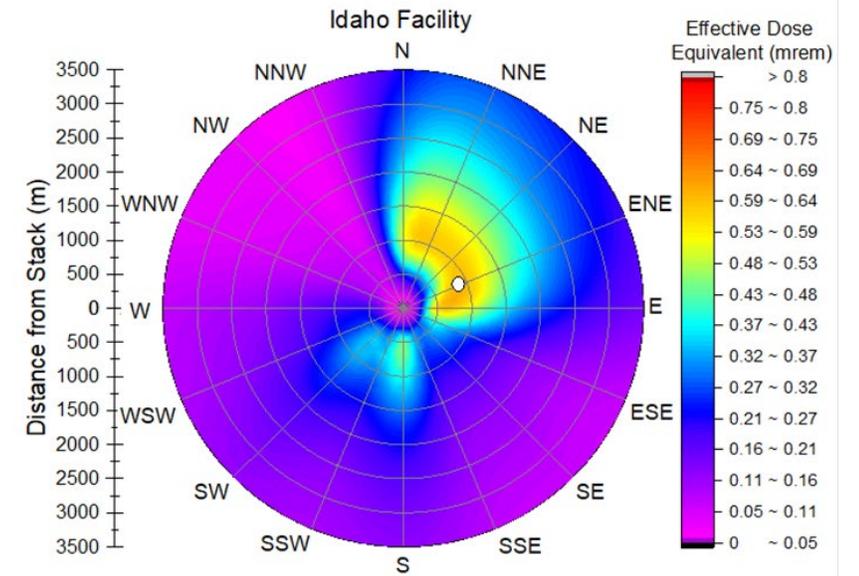
# Why off-gas treatment?

- Primary volatile radionuclides:  $^3\text{H}$ ,  $^{14}\text{C}$ ,  $^{85}\text{Kr}$ ,  $^{129}\text{I}$
- Semi-volatiles: ruthenium, technetium, others
- Speciation and volatile partitioning varies according to processing flowsheet

## US regulations have two aspects:

- (1) Limit Ci amounts of  $^{85}\text{Kr}$  and  $^{129}\text{I}$  discharge
- (2) Limit dose to public on a whole-body and thyroid basis

➤ Governing regulations are 40 CFR 190, 40 CFR 61, and 10 CFR 20. (EPA and NRC)



**Air dispersion modeling to determine the dose from iodine emissions**

S. BRUFFEY et al., "Requirements and Conceptual Design of Off-gas Systems for the Reprocessing of Metallic Fuels," ORNL/TM-2020/1668, Oak Ridge National Laboratory, Oak Ridge, TN (2020).

# Specific Metrics for Off-gas Systems

- **Iodine-129 release limited to 0.005 Ci/GW<sub>e</sub> · y**
  - Expect to retain, at minimum, 99.5 to 99.9% within the facility
- **Kr-85 release limited to 50 Ci/GW<sub>e</sub> · y**
  - Expect to capture 70-95% within the facility
- **Total dose to the public from all facility emissions:**
  - 25 mrem/whole body; 75 mrem/thyroid

# What is the off-gas baseline for aqueous processing?

## Key unit operations:

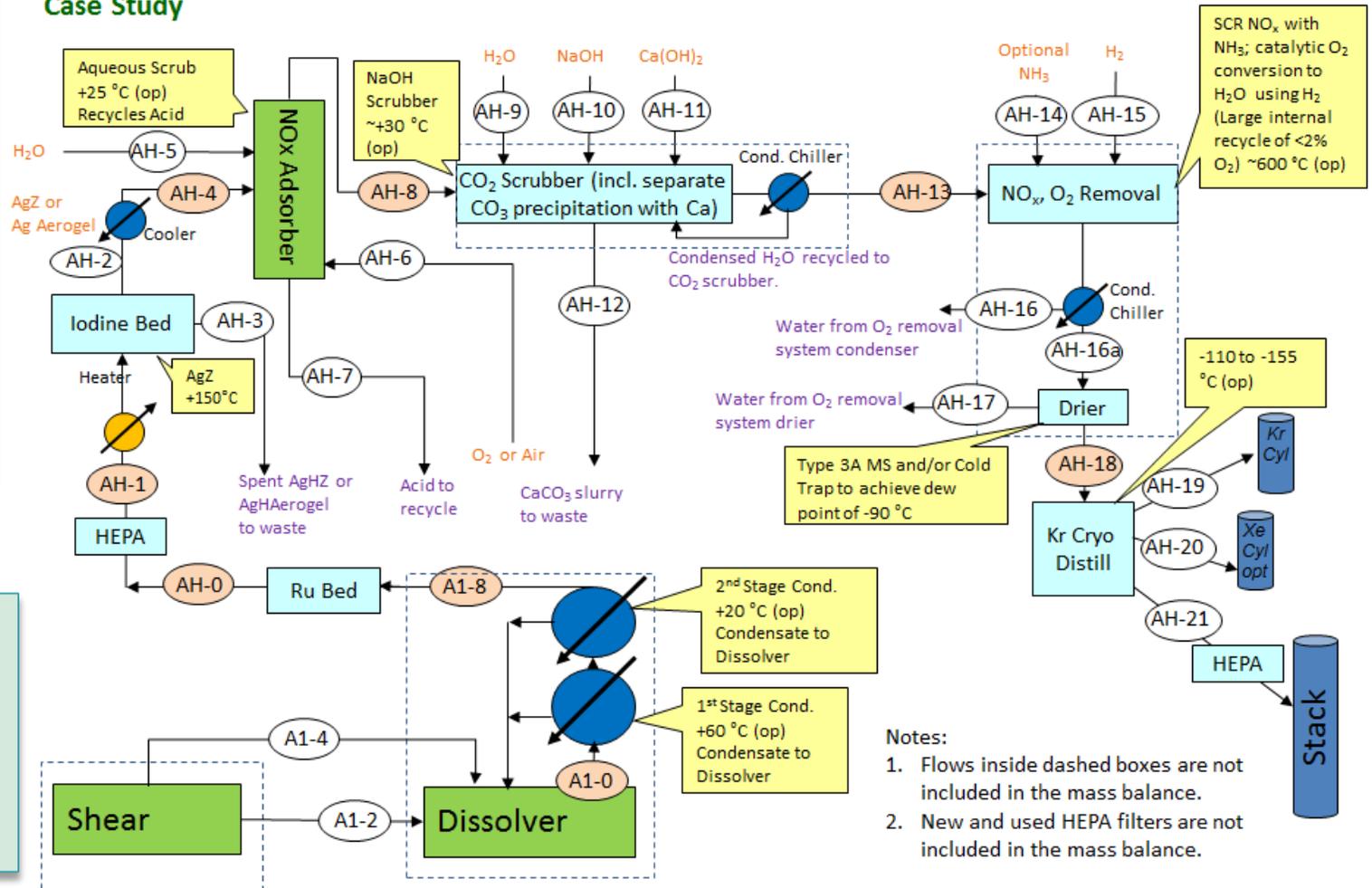
- Ru removal
- Iodine removal
- NO<sub>x</sub> removal
- CO<sub>2</sub> removal (optional)
- NO<sub>x</sub>, O<sub>2</sub> removal
- Kr/Xe condensation or separations

## Notes:

- (1) Tritium distributes through plant (aq. and gas)
- (2) Kr/Xe 1:10 ratio – separations decreases waste by 10×

## Aqueous Head-end and Dissolver Off-gas Systems (No TPT)

### Case Study



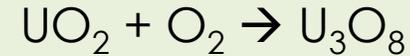
### Notes:

1. Flows inside dashed boxes are not included in the mass balance.
2. New and used HEPA filters are not included in the mass balance.

# Alternatives have typically included pretreatment:

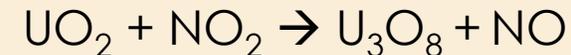
- **Voloxidation**  
(removal of  $^3\text{H}$  before dissolution)
- **Advanced voloxidation**  
(removal of I and  $^3\text{H}$  before dissolution)
- **Direct dissolution**  
(advanced volox, no dissolver)
- **High temperature voloxidation**  
(OREOX, DUPIC) – removes semi-volatiles

## Standard O<sub>2</sub> Oxidation



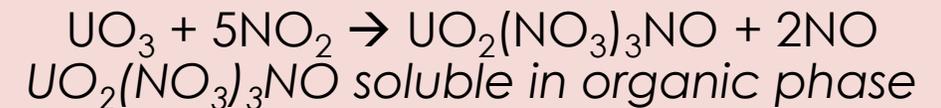
**Off-gas:**  $^3\text{H}_2\text{O}$ , some semi-volatiles, Kr/Xe  
**Treatment:** Water removal, filtration

## Advanced NO<sub>2</sub> Oxidation



**Off-gas:**  $^3\text{H}_2\text{O}$ ,  $^{129}\text{I}$ , Kr/Xe, less semi-volatiles  
**Treatment:** More complex

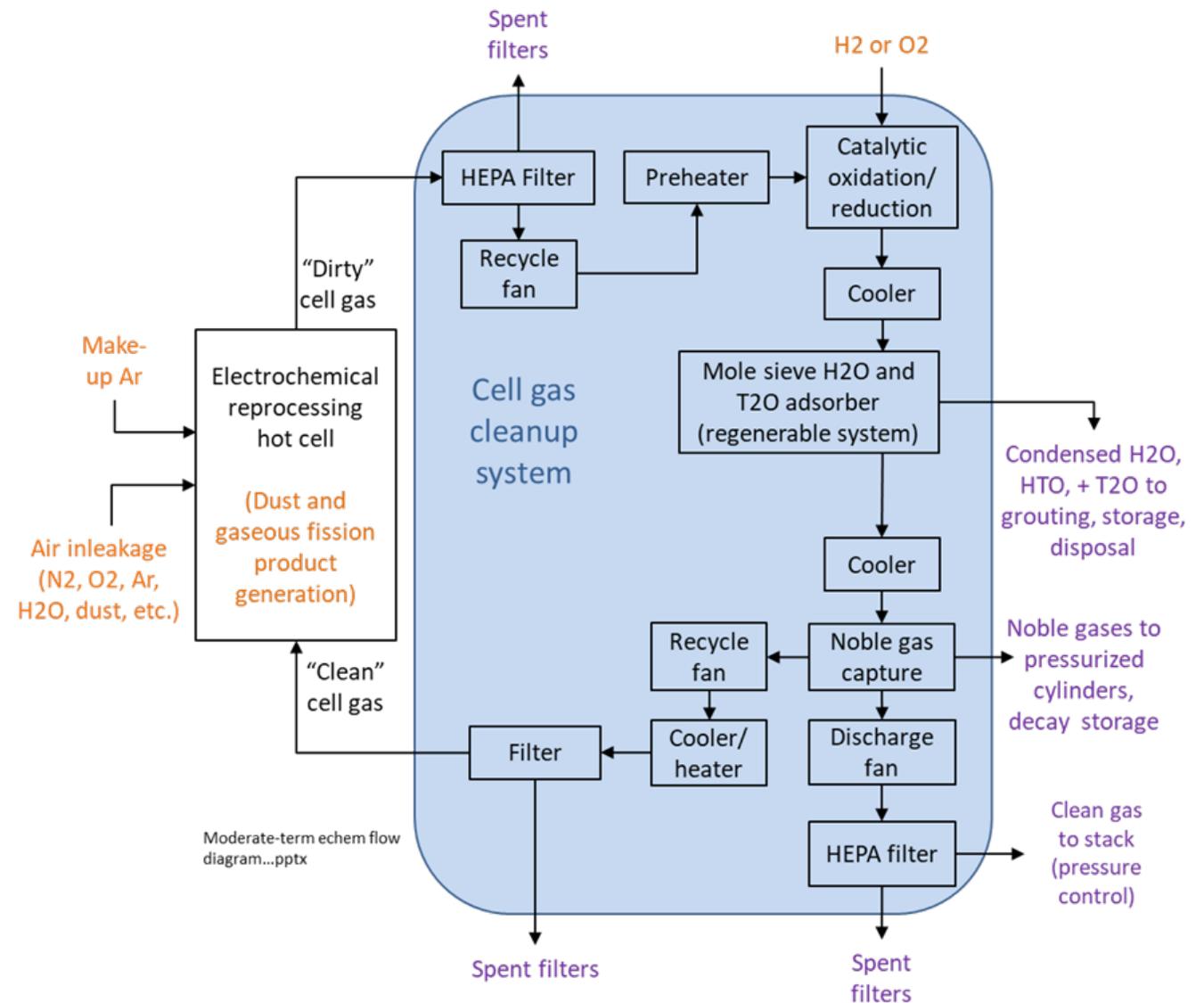
## Direct Dissolution



**Off-gas:** Eliminate DOG, add Volox-OG

# What's the off-gas baseline for pyroprocessing?

- Here, assume the electrorefiner emits to the argon hot cell
- No  $^{14}\text{C}$ , less iodine
- Other operations, such as salt distillation, may require additional iodine management



# Other off-gas thoughts:

- **Consider other effluents: A balancing act**
  - Control liquid effluents well, higher ceiling on gaseous effluents
  - Control iodine well, limit need for additional controls for other volatiles
  - There is always opportunity for less costly, higher efficiency capture media
- **Consider fuel age:**  $^3\text{H}$  and  $^{85}\text{Kr}$  requirements decrease with fuel age, leaving a higher dose-ceiling for iodine (must always control to Ci/GWd limits)
- **Consider how capture processes can integrate** with waste management
- **Target flexibility:** capture processes that are broadly applicable across multiple processing flowsheets
- **Consider waste forms:** waste volumes generated from off-gas capture are traditionally high volume.
  - Integrate the process with the final waste form
  - Better iodine waste forms are needed, better Kr storage forms are needed

# Summary:

- Off-gas/Head-end processing contribute significantly to facility capital cost and O&M
- Alternative head-ends, simplified off-gas treatments, and better secondary waste management can yield improved operations and cost benefit
- Focus on smaller equipment, earlier removal of activity, decreased shielded space

# Questions?



